ALUM AND LIME DOSING CONTROLLERS FOR WATER TREATMENT PLANT

A dissertation submitted to the

Department of Electrical Engineering, University of Moratuwa
in partial fulfillment of the requirements for the
degree of Master of Science

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L.P. HETTIARACHCHI

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Supervised by: Dr. Palitha Dasanayake

Department of Electrical Engineering University of Moratuwa, Sri Lanka

December 2007

91205



DECLARATION

The work submitted in this dissertation is the result of my own investigation, except where otherwise stated.

It has not already been accepted for any degree, and is also not being concurrently submitted for any other degree.

L.P. Hettiarachchi

Date: 11.02.2008

I endorse the declaration by the candidate.

UOM Verified Signature

Dr. Palitha Dassanayake

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Abstract

Many techniques are applied to the control of Alum and Lime commonly termed as coagulant dosing in a drinking water treatment plant. Coagulant dosing rate is non linear correlated to raw water parameters such as turbidity, conductivity, pH, temperature, etc. Manual method called Jar testing is used to decide the Alum and Lime dosage. However in practical situation, Jar testing is carried out maximum three times per day. But the parameters of water sources are continuously changing specially on rainy days. Therefore overdosing and underdosing of Alum and Lime are normally occurred. Excessive coagulant overdosing leads to increase treatment costs and human health problems, while underdosing leads to failure to meet the water quality targets and less efficient operation of the water treatment plant. It means that important requirement arises to automate the system with optimum coagulant dosage.

The research is aimed to propose an alternative to the jar test allowing for an on line determination of optimal coagulant dosage from raw water characteristics and design a system for feeding Alum and Lime automatically with a monitoring display.

The reasonable assumption made by this research is, except turbidity and pH value, other parameters are almost same throughout year. After analyzing thousand number of jar test results with corresponding turbidity values and pH value of incoming water, it was found turbidity value of raw water and the dosage of Alum has a relationship and pH value of raw water and the dosage of Lime has another relationship. Relationship of turbidity value of raw water and the dosage of Alum is second order polynomial. However pH value of raw water and the dosage of Lime have stepwise relationship. And also actual values of three hundred situations were taken and applied to check the validity of relationships and it is proved that the relationships which has obtained are well suited to develop the automation system.

Next objective is designing of hardware and software part of controller of an automotive system to dose Alum and Lime using the relationship. PIC16F876 microcontroller is selected as the controller; it made the task easier. Since PIC16F876 has 8-bit with analogue to digital converters, it handled analogue output of turbidity sensor and pH sensor. In this project MAX 7219 display driver IC could be easily interfaced with microcontroller by using three wires (SDO, SDI and SCLK) and LOAD (CE) which is common today named as Serial Peripheral Interface (SPI). The PIC16F876 chip is in electrical erasable packaged version (FLASH), and it helped for programming several times for testing our object before implementing.

Finally complete control and feeding system for Alum and Lime was designed. Value of turbidity was measured by a turbidity sensor. That value was taken to the microcontroller that decides the Alum dosage and changes the valve position using stepper motor accordingly. Either increment or decrement of the value of turbidity by 10 makes the changing of valve position in ADC. Either increment or decrement of the value of pH value by 0.1 makes the changing of valve position in LDC. Using MAX7219 IC current value of turbidity and current value of pH are displayed in ADC and LDC respectively.

Key features of the system are simple relationships constructed to find optimum coagulant dosage and ability of handling practical situations of water treatment plants using automation system with microcontrollers.



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My foremost duty is to express my sincere gratitude to my supervisor, Dr. Palitha Dassanayake, Senior Lecturer, University of Moratuwa, for his great insights, perspectives, guidance and sense of humor.

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List of Principal Symbols

Table

ANN Artificial Neural Network **FRBS** Fuzzy Rule Based System Streaming Current Detector SCD **ADC** Alum Dosing Controller LDC Lime Dosing Controller A/D Analogue to Digital Self Organizing Map SOM Universal Exhaust Gas Oxygen **UEGO** Liquid Crystal Display LCD Universal Serial Bus USB PLC Programmable Logic Controllers Programmable Intelligent Computer PIC



Chapter 1

Introduction

1.1 Background

Water treatment costs five to ten rupees per cubic meter. However maintaining the standards of water quality is a must in water sector. Therefore it is very important to make standard quality of water at minimum cost. Automating systems in water treatment is a successful solution for fulfilling that requirement.

The water that is found in rivers and reservoirs are usually not suitable for drinking. The rivers and reservoirs are polluted by the activities of man and animals. The effluents of the industries situated along the water source, domestic wastes, storm water and sewage-all enter the water source through a system of drains and waterways.

The purification or the treatment process consists of five major steps. They are Aeration, Addition of chemicals, Sedimentation, Filtration, and Disinfection. Introducing Oxygen into water is called Aeration. By this means the taste, colour and odour causing substances and gasses are removed. Process of Addition of chemicals is also called a process of coagulation and flocculation. Lime and Alum are the chemicals used in water treatment. When chemicals are added to water, it reacts with soil and clay particles, microorganism and other substances. This is called coagulation. These particles associate with similar particles to form big flocs. The process is called flocculation. The flocs when it is heavy sink to the bottom. The result is clear water at the top. The third step is sedimentation. The flocs as stated above are formed in large sedimentation tanks. Clear water is found at the surface of the tank. This water is sent into the sand filters through network of channels. The suspended solids and some microorganisms are removed by filtration process. Disinfection is the last step. This is also called as chlorination as it uses chlorine gas to disinfect water. Chlorine is a strong oxidizing agent and it destroys pathogens- that are disease causing organisms like Bacteria remaining in the water.

After designing and constructing water treatment plant in proper way, main operational activity that affects water quality is adding of quantity of chemicals. Excessive amount of Alum/Lime dosing leads to public health matters and chemicals are very expensive since those chemicals are imported. Alum costs forty thousand rupees per metric ton and lime costs fifteen thousand per metric ton.

Less amount of coagulant dosing causes poor quality of water and decrement of efficiency of rest of stages of water treatment. Therefore it is very significant to dosing optimum amount of chemical.

Optimum amount of Alum/Lime is decided by a laboratory test called jar test. But this traditional method takes some time to give the readings. At that time parameters of water is changed. Therefore identification of a new method for deciding the optimum dosage is needed for automating the Alum/Lime feeding system.

After doing the jar test dosage is changed manually. Therefore this whole procedure relies on manual intervention. In this case, automating the system with suitable on line measurement can reduce manpower and chemical costs and improve compliance with treated water quality targets.

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1.2 Problem Backgroundb.mrt.ac.lk

The water industry is facing increased pressure to produce higher quality treated water at a lower cost. The coagulation – flocculation process is a major step in the production of potable water, allowing the removal of colloidal particles. The main difficulty is to determine the optimum coagulant dosage related to the incoming water characteristics. Excessive coagulant overdosing leads increased treatment costs and public health concerns, while underdosing leads to failure to meet the water quality targets and less efficient operation of the water treatment plant.

For the moment manual method called jar testing is available to predict optimum coagulant dosage rate. Jar testing involves taking raw water sample and applying different quantities of coagulant to each sample. After a short period of time each sample is assessed for water quality and the dosage that produces the optimal result is used as set point. Operators change the dose and make a new jar test if the quality of treated water changes.

Disadvantages associated with jar testing are the necessity to perform manual intervention, and lack of adaptation to abrupt changes of water characteristics.

After getting the jar test results manual controlling system is used to change the dosage. Therefore whole procedure is done by manual control and it leads to wastage of expensive chemicals, failure to meet water quality targets and reduced efficiency of sedimentation and filtration processes.

1.3 Research Objective

The main objectives of this research is to propose an alternative to the jar test allowing for an on line determination of optimal coagulant dosage from raw water characteristics and design a system for feeding Alum and Lime automatically with a monitoring display.

1.4 Organization of Dissertation

This report consists of five chapters. The first chapter discusses the background of the study, shape of the problem and goals which are going to achieve. The second chapter is the literature review. It consists of historical review of coagulant dosage controllers in water treatment plants and presents the state of the situation.

In chapter three under research design and methodology, it has discussed method of data collection and method of pull off configuration of the system, layout diagrams and components of the system. The chapter four is discussing the research findings. It includes equations for optimum Alum and Lime dosage and system algorithm, software and hardware developed.

The final chapter which is chapter five discussed the conclusions and recommendations.

The report ends with References and Appendices.

Chapter 2

Literature Review

Alum and lime dosing controlling in water treatment plants is a developing area. In Sri Lanka context, dearth of literature can be readily retrieved. However experimentations and projects are done and ongoing worldwide to some extent.

This chapter presents literature on Alum and Lime dosing controlling in water treatment plants, microcontroller based systems, water quality parameters, jar test in to water treatment process, covering wide range of text books, journal articles, thesis reports, reputed websites and etc.

2.1 Historical Review

Studies were carried out related to Alum and Lime (coagulant) dosing controlling in water treatment plants and followings describes about them.

Various types of intelligent methods used in dosing control of water treatment are one of a study area popular in water sector.

In a research article by Juuso et al., (2003), was addressed the Linguistic equations method, an intelligent method using to define new operating point of chemical dosing according to the quality or amount of incoming water. In this paper data were recorded from a real water purification process and two kinds of models were derived for the process by using this information, namely steady state and a dynamic model. Static model defines the new operating point and the dynamic model predicts a reasonable dosing rate for the chemicals in the current working point. They also stated that linguistic equation helped them handled quite small data since linguistic equation do not necessarily need expert knowledge unlike fuzzy systems and do not have to be as large as for neural network. They concluded that dynamic model needs improvement before using it in the controller design.

An integrated coagulant dosing system based on unsupervised and supervised neural network models, as well as various statistical techniques are introduced in the research done by Valentin et al., (2000). The system developed includes raw water validation and reconstructed based on a Kohonen self-organizing feature map, and prediction of coagulant dosage using multilayer perception. The performance of the network was dependent on the quality and completeness of data provided for system training. Also they stated that continuous updating of training data would certainly improve the performance of the system.

Valentin and Denoeux's (2002) research was focused on a neural network – based software sensor for coagulation control in a water treatment plant. It described the application of artificial neural network techniques to coagulation control in drinking water treatment plants. The software sensor developed was a hybrid system including a self-organizing map (SOM) for sensor data validation and missing data reconstruction, and a multi-layer perception (MLP) the coagulation process. They also stated that this system can handled various sources of uncertainty such as atypical input data, measurement errors and limited information content of the training set.

In the research article by Baxter et al., (2002) was discussed a methodology for developing with a handful of time and successful ANN models of drinking water treatment process. They presented that the ANN modeling methodology allows utilities to develop multiple – variable nonlinear models of complex unit processes such as coagulant dosing control in a simple sequential fashion. Their conclusion was, ANN modeling methodology allowed utilities to develop multiple variable nonlinear models of complex unit processes in a simple sequential fashion and with improved usability. And they also stated that ANN technology will play a larger role in helping utilities meet customer and regulatory demands on finished water quality through improved modeling in future.

Project Report, Delft 2000 was reviewed the principles of various types and architectures of neural network and fuzzy adaptive systems and their applications to integrated water resources for management. It concluded that fuzzy-based methods are applied for identifying optimal control action of wastewater treatment plant, determining optimal dosage thereof and determining leakage. Combination of expert knowledge was also applied. Fuzzy rule based systems (capable of building rules automatically) had been applied for determining optimal control action and filling in the measured data.

In the research article done by Masson et al., (1999) was addressed another software sensor design, based on empirical data ecological modeling and it stated that process monitoring and control in water treatment relies heavily on accurate and reliable sensor information. Whereas many process parameters can be measured continuously using relatively simple and cheap physical sensors, the determination of certain quantities of interest requires costly laboratory analysis which cannot be performed on-line. They also stated that such high level information could be inferred from available measurements of observable quantities using a statistical model called as software sensor.

Both research article done by Mirsepassi et al., (1995) and Evans et al., (1998) were addressed the potential effectiveness of an approach of building a software sensor for on-line determination of optimal coagulant dosage from raw water characteristics such as turbidity, pH. conductivity, etc., based on artificial neural network.

Studies done by Bernazeau et al., (1992) and Dental (1995) emerged an automatic device called a streaming current detector (SCD) in coagulation monitoring and control. This device was based on the measurement of the net residual charge surrounding turbidity and colloidal particles in water. It required a set point to be entered, assumed to represent an optimum water quality standard. Streaming current values above the set point indicated an excess of coagulant, while values below the set point indicated insufficient coagulant dosage for full flocculation to occur. A jar test needs to be carried out to determine the set point. They also stated that this method is costly and limited efficiency for certain types of raw water quality.

In the research article done by Trautmann and Denoeux (1995) was addressed applications of self organizing maps (SOM's) to water quality monitoring. The SOM model combined the goals of projection and clustering algorithms and might be seen as a method for automatically arranging high – dimensional data. It used at the same time to visualize the clusters in a data set, and to represent the data on a two dimensional map in a manner that preserves the non linear relations of the data items, nearby items being mapped to neighboring position on the map.

Studies on coagulant control and optimization done by Lind, (1994) were focused on both manual and automatic methods to predict optimum coagulant dosage rate.

The article written by Pask, (1993) has illustrated budget saving of selecting optimum chemical dosage in water treatment by jar test. According to that for accurate jar test it took minimum one and half hours.

Chazel's (2006) research on controlling oxygen sensors with an automotive microcontroller had addressed the feasibility of controlling a UEGO sensor directly from a microcontroller, with a low level of cost and complexity. The use of a microcontroller was particularly adequate for this application. He also stated that the two regulation loops were easily implemented on the microcontroller and interfaces were immediately removed by software. By using microcontroller electronics came to simple and only basic components were required since all the regulation tasks were handled by microcontroller.

The article written by Jahan, (2003) was discussed the parameters that characterize water quality, measuring water quality parameters using analytical equipment and principle of coagulation flocculation process. Also he stated that turbidity, pH value, temperature, conductivity, dissolved oxygen and UV's absorption were the main parameters for coagulation flocculation process. Turbidity detection was used to measure the total solids content whereas UV's absorption detection could be employed to measure the total content of dissolved organic matter.

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PIC Microcontroller Solutions vincluding the microchip advantage, flexible programming options, PIC microcontroller migration strategy, PIC microcontroller product architectures (Baseline architecture, Mid-range architecture, High performance architecture), general purpose microcontroller features (Low power nanoWatt technology, high pin count high density memory, low pin count and space constrained, PIC microcontrollers with high voltage support and fan control capabilities), PIC microcontrollers with an integrated LCD module, PIC microcontrollers with integrated USB and PIC microcontrollers with Ethernet capabilities were demonstrated in http://www.microchip.com website, (2007).

Microcontroller Interfacing Techniques including advantages, disadvantages and examples of digital I/O control and monitoring, voltage based control and monitoring, parallel and serial bus, Asynchronous communication (1-wire, Rs232/RS485, Ethernet) and Synchronous communication (2-wire, 4-wire) were demonstrated in http://www.bipom.com website, (2007).

Project done by Arthur C. Clarke Institute for Modern Technologies, (2005) was revealed PIC microcontrollers are low cost, industry standard high performance and 8-bit with analogue to digital converters. They used PIC16F873 for their project of length counter.

Emunrud's (2002) research on Programmable Logic Controllers has addressed on the history of PLC development, the components that make up PLCs, need and current effort to standardize PLCs, advantages and disadvantages compared to other control systems. It concluded that the one major disadvantage to PLC was lack of standardization and this caused much confusion if the PLC used for an application was replaced by one from a different manufacturer, or if a PLC programmer was replaced by a person with a different understanding of PLC programming.



Chapter 3

Research Design and Methodology

3.1 Introduction

Main objective of this research is to develop models to automate Alum and Lime dosing for water treatment plant and to predict relationships between measuring parameters (turbidity and pH value) of water and amount of dosage of Alum and Lime.

3.2 Assumptions

Alum and Lime dosage is depends on water parameters of Turbidity, pH value, temperature, conductivity, dissolved Oxygen, UV's absorption, etc. However considering one water source conductivity, dissolved oxygen, temperature and UV's absorption remain same. Turbidity, number of particles in water is the main cause for optimum Alum dosage and pH value is the main cause for optimum Lime dosage.

Therefore Ambatale Water treatment plant which distributes water to Colombo area is selected for this research and followings are the basic information of it.

Year Commissioned

1966 (Old Plant)

1994 (New Plant)

Water Source

Kelani River

Water Intake

02 Pump Houses (Old & New)

577,000 cum per day

Sedimentation

05 Tanks capacity 61,300 cum each

Tanks

04 Tanks capacity 45,000 cum each

• Filters 26 (18+8) Rapid Gravity Sand

Filters

• Chemicals : Alum $Al_2(SO_4)_3$. $14H_2O$

Lime Ca(OH) 2 Chlorine gas Cl₂

• Water Storage : 03 Tanks (91,000, 4200, 6600 cum)

• Production per day : 470,000 cum (105 million gallons)

• Production Capacity 500,000 cum per day

(maximum)

Water Treatment Operation University of Moratuwa, Sri Lanka.

The treatment plant gets its water supply from Kelani River. Water treatment involves physical chemical and biological processes that transform raw water into drinking water. Aeration, addition of chemicals, sedimentation, filtration and disinfection are the major steps. Aeration means air (oxygen) is introduced to water. By this means, the taste, colour and odour causing substances and gases are removed. Then chemicals, lime and alum are adding. When chemicals are added to water they react with soil and clay particles, microorganisms and other substances. This is called coagulation. These particles associate with similar particles to form big flocs. This process is called flocculation. The floes when it is heavy sink to the bottom. The result is clear water at the top. Then the sedimentation process is carried out. The flocs as stated above are formed in large sedimentation tanks. These clarification tanks are called pulsators, pre-treaters and centriflocs. Clear water is found at the surface of the tanks. This water is sent into the sand filters through a network of channels. The next step is filtration. Water is filtered through the rapid gravity sand filters. The suspended solids and some microorganisms are removed by the process. After that Alum is again added to do the pH correction. This is called as addition of post Lime. Last step of the water treatment process is disinfection. This is also called chlorination as it uses chlorine gas to disinfect water. Chlorine is a strong oxidizing agent and it destroys pathogens; that is disease causing organisms like bacteria remaining in the water.

Figure 3-1 shows layout diagram of Ambatale water treatment plant.

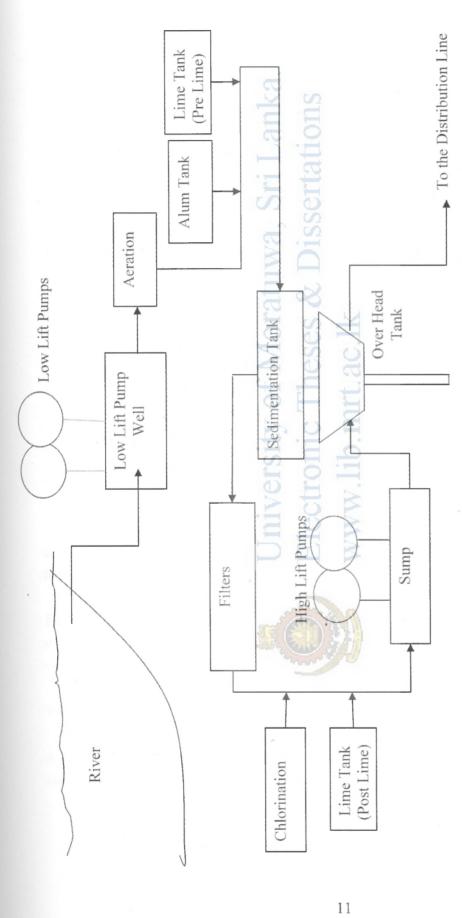


Fig 3-1 Layout Diagram of Ambatale Water Treatment Plant

3.3 Data Collection

This research is based on field data and experimental results using real data. One thousand number of jar test results for raw water were recorded (Appendix-A) to predict a relationship between measuring parameters (turbidity and pH value) of water and amount of dosage of Alum and Lime. Three hundred numbers of experiments are done to check the validity of results (Appendix-B).

3.4 Design of the System

Design of the Controller

This design is for controlling alum and lime dosing according to the turbidity and pH value of the incoming water. At the same time the system should indicate the value of turbidity and pH value in a display unit.

Features of the system are described below.

Since the dosing controller is designed using a microcontroller it allows for the flexibility of ease of operation.

The changing of dosage of Alum is occurred where the difference of turbidity value equal to ten (10) according to the initial value of turbidity. Then new value of turbidity is the initial value for next time.

The changing of dosage of Lime is occurred where the difference of pH values equal to point one (0.1) according to the initial value of pH value. Then new value of pH value is the initial value for next time.

Value of turbidity, value of pH, current dosing rates of alum and lime are indicated.

A master reset button can be used in case where the system locks-up due to some unpredictable event.

Selection of the Main Controller

To control the system, a microcontroller, a programmable logic controller or a PC using some form of I/O can be used.

Microcontrollers generally can be classified into 8-bit, 16-bit, and 32-bit family based on the size of their arithmetic and index register(s). It generally consists of ROM(Read Only Memory), RAM(Random Access Memory), Stack Pointers, Registers, Accumulator, Input/Output Ports, Timers, Analog to Digital Converter(ADC), Digital to Analog Converter(DAC), UART or SPI (for communication purposes). Some have special built in features that comes with Liquid Crystal Display Driver (LCD) that will enable them to drive LCD displays, EEPROM (Electrical Eraseable Programmable Read Only Memory) which is a non volatile memory that will enable it to store data permanently.

It can be implemented using high level language or assembly language. Clock speed determines how much processing can be accomplished in a given amount of time by the MCU. Some have a narrow clock speed range. Sometimes a specific clock frequency is chosen to generate another clock required in the system, e.g. for serial baud rates.

The processing technology of the microcontroller is N-channel metaloxide semiconductor (NMOS) or high-density complementary metal-oxide semiconductor (HCMOS). In HCMOS, signals drive from rail-to-rail, unlike earlier NMOS processors. Since these criteria can significantly affect noise issues in system design, HCMOS uses less power and thus generates less heat. The design geometries in HCMOS are smaller, which permit denser designs for a given size and thus allow higher bus speeds. The denser designs also allow lower cost, for more units can be processed on the same sized silicon wafer. For these reasons, most MCUs today are produced using HCMOS technology.

The advantages of microcontroller are that all MCUs have on-chip resources to achieve a higher level of integration and reliability at a lower cost. An on-chip resource is a block of circuitry built into the MCU which performs some useful function under control of the MCU. Built-in resources increase reliability because they do not require any external circuitry to be working for the resource to function. They are pre-tested by the manufacturer and conserve board space by integrating the circuitry into the MCU.



Some of the more popular on-chip resources are memory devices, timers, system clock/oscillator, and I/O. Memory devices include read/write memory (RAM), read-only memory (ROM), erasable programmable ROM (EPROM), electrically erasable programmable ROM (EEPROM), and electrically erasable memory (EEM). The term EEM actually refers to an engineering development version of an MCU where EEPROM is substituted for the ROM to reduce development time.

Timers include both real-time clocks and periodic interrupt timers. Other timer functions include timer compare and/or input capture lines.

I/O includes serial communication ports, parallel ports (I/O lines), analog-to digital (A/D) converters, digital-to-analog (D/A) converters, liquid crystal display drivers (LCD), and vacuum fluorescent display drivers (VFD).

Other built-in resources may include computer operating properly (COP) watchdog system which can be hardware or software based.

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A microcontroller is a single integrated circuit. Integrating the memory and other peripherals on a single chip and testing them as a unit increases the cost of that chip, but often results in decreased net cost of the embedded system as a whole. Even if the cost of a CPU that has integrated peripherals is slightly more than the cost of a CPU + external peripherals, having fewer chips typically allows a smaller and cheaper circuit board, and reduces the labor required to assemble and test the circuit board.

Microcontrollers are useful to the extent that they communicate with other devices, such as sensors, motors, switches, keypads, displays, memory and even other microcontrollers. Many interface methods have been developed over the years to solve the complex problem of balancing circuit design criteria such as features, cost, size, weight, power consumption, reliability, availability, manufacturability.

Many microcontroller designs typically mix multiple interfacing methods. In a very simplistic form, a micro-controller system can be viewed as a system that reads from (monitors) inputs, performs processing and writes to (controls) outputs.

PLCs are typically industrial processes in manufacturing where the cost of developing and maintaining the automation system is high relative to the total cost of the automation, and where changes to the system would not be expected during its operational life.

Very complex process control, such as used in the chemical industry, may require algorithms and performance beyond the capability. Very high-speed or precision controls may also require microcontroller solutions.

PLCs are not very good at handling large amount of data, or complex data. Microcontrollers are better for that. PLCs are also not very good with databases or displaying data.

Main Controller

The main controller is mainly established by using PIC16F876 microcontroller which is shown by Fig 3-2. This microcontroller has the following features that are best suited to conduct the task.

It process low cost, industry standard high performance and 8-bit with analogue to digital converters.

The support for a variety of range of input/output functions, and this microcontroller allow the user to determine whether to use a certain pin as input or output.

There are 192 bytes of RAM and has 22 input/output pins in additional several peripheral features such as timers, counters, etc.

There is also a serial port it capable of being programmed easily and interfaced with computer via standard RS232 port.

In this project MAX 7219 display driver IC can easily interfaced with microcontroller by using three wires (SDO, SDI and SCLK) and LOAD (CE) which is common today named as Serial Peripheral Interface (SPI).

The varieties of software tools are available for developing and debugging source code for the controller. The MPLAB software is used for developing the system because it is windows based an easy software development in 8-bit microcontroller.

The PIC16F876 chip is in electrical erasable packaged version (FLASH), and it is suitable for programming several times for testing our objective is implemented.



Fig 3-2: Pin Configuration of PIC16F876

Display Driver Unit

The display driver unit consists of 7-segment displays for visualizing the value of turbidity (or pH value) of the incoming water and the current dosage rate of Alum (or Lime). The MAX7219 display driver chip can derive multiplexed 7-segment displays, and convenient 3-wire serial interfacing with main controller. This IC is compact, common cathode display driver up to 8-digits. Included on chip is a BCD code-B decoder, multiplexer, scan circuitry of the display drivers, and on 8×8 static RAM that store each digit. The circuit of the display driver unit is shown in Fig 3-3.

Sensor Unit

The sensor is established in raw water just before adding Alum (or Lime) to measure the turbidity (or pH value). The turbidity sensor gives the interrupts to the microcontroller when the turbidity value is increased or decreased by 10 in ADC. The pH sensor gives the interrupts to the microcontroller when the turbidity value is increased or decreased by 0.1 in LDC.

Selected turbidity meter, WQ710 is perfectly matched for the design since it can be inserted into low pressure pipes by using standard compression coupler for turbidity monitoring and readings are giving every three seconds. It shows that output currents at the maximum turbidity values close to 20mA, so that it is easy to work with microcontroller.

Selected pH sensor, PH-BTA has an Ag-AgCl combination electrode with a range of 0 to 14 pH units. It is a high quality electrode for water quality monitoring. And also it is very compatible with microcontroller interfacing.

Stepper Motor

The stepper motor is to change the position of valve. Either increment or decrement of the value of turbidity by 10 valve position is changed according to the pre defined values in ADC. Either increment or decrement of the value of pH value by 0.1, valve position is changed according to the pre defined values in LDC.

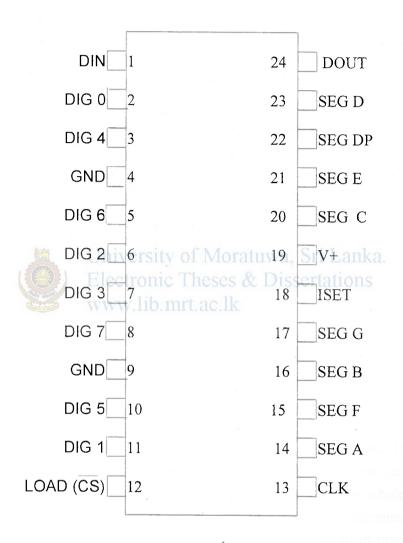


Fig 3-3: Pin Configuration of MAX7219

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Stepper motors are commonly used in measurement and control applications. Following features are common to all stepper motors make them ideally suited for these types of applications.

Stepper motors are brushless. The commutator and brushes of conventional motors are some of the most failure – prone components and they create electrical arcs that are undesirable or dangerous in some environments.

Stepper motors will turn at a set speed regardless of load as long as the load does not exceed the torque rating for the motor.

Stepper motors move in quantified increment or steps. As long as the motor runs within its torque specification, the position of the shaft is known at all times without the need for a feedback mechanism.

Stepper motors are able to hold the shaft stationary. (Holding torque)

Stepper motors have an excellent response to start – up, stopping and reverse.

3.5 Methodology of the research

The study is based on primary data collection of jar test unit data. It is taken from Ambatale water treatment plant. Three no of jar tests are carried out per day. Data from May, 2006 to April, 2007 were recorded. Since it includes whole year both dry and rainy conditions are covered. Turbidity and pH value of incoming water, Alum requirement pre Lime requirement and post Lime requirement in ppm consist in the sample.

After analyzing the data, equations for optimum dosage of Alum and pre Lime with Turbidity and pH of incoming water are found respectively. Then three hundred real situations are taken and applied new results to them. There turbidity, pH value of raw water and turbidity, pH value at settled water at pulsators, pre-treaters and centriflocs, turbidity, pH value of filtered water and turbidity, pH value of final water are measured. Above procedure was done to check the validity of results.



Then the system is designed using PIC16F876 microcontroller as the controller. Source codes are constructed using Assembly codes. Value of turbidity is measured by a turbidity sensor. That value is taken to the microcontroller and it makes the decision of the Alum dosage and changes the valve position using stepper motor accordingly. Either increment or decrement of the value of turbidity by 10 makes the changing of valve position in ADC. Either increment or decrement of the value of pH value by 0.1 makes the changing of valve position in LDC Using MAX7219 IC value of current value of turbidity and current value of pH are displayed in ADC and LDC respectively.

Block diagram of the system is shown in Fig 3-4.

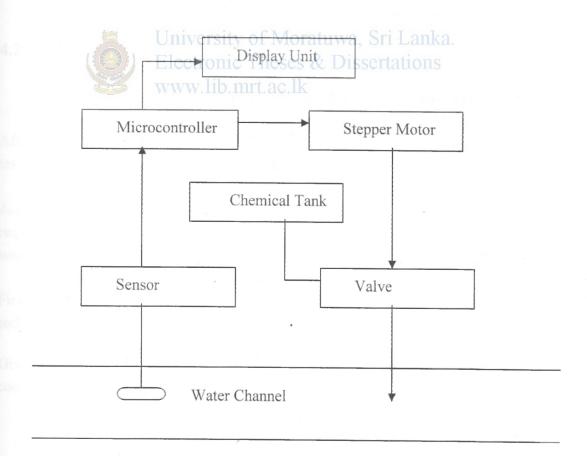


Fig 3-4: Block Diagram of the System

Chapter 4

Research Findings

4.1 Introduction

This chapter discussed the relationship of Alum dosage with turbidity for ADC, the relationship of Lime dosage with pH value for LDC, automotive systems of Alum dosing and Lime dosing and hardware design of the system and software design of the controller.

4.2 Constructed Relationships

Relationship of Alum dosage with turbidity for ADC

After analyzing of turbidity of raw water and Alum dosage which is measured by Jar test from May, 2006 to April, 2007 following graphs were obtained.

According to the jar test results value of turbidity and corresponding Alum requirement is plotted in x-y scatter chart in Microsoft Excel. Then a "best-fit" line was drawn through the data points.

First, best fit straight line was considered. It is shown in Fig 4-1. Linear regression technique is powerful tool to show that the data points are fit into a straight line.

Given a set of data (x_i, y_i) with n data points, the slope, y-intercept and correlation coefficient, r, can be determined using the following:

$$m = \frac{n\sum (xy) - \sum x \sum y}{n\sum (x^2) - (\sum x)^2}$$

$$b = \frac{\sum y - m \sum x}{n}$$

$$r = \frac{n\sum (xy) - \sum x\sum y}{\sqrt{\left[n\sum \left(x^2\right) - \left(\sum x\right)^2\right] \left[n\sum \left(y^2\right) - \left(\sum y\right)^2\right]}}$$

(The limits of the summation, which are i to n, and the summation indices on x and y have been omitted.)

Correlation coefficient, r can take on values from 0 to 1, where 1 means there is a perfect match and means that all the points are on the line exactly.

(Most statistical texts show the correlation coefficient as "r", but Excel shows the coefficient as "R". Whether it is as r or R, the correlation coefficient gives us a measure of the reliability of the linear relationship between the x and y values).

According to the Fig 4-1,

• R-squared, $r^2 = 0.7923$

• Correlation Coefficient, r = 0.8901

Also the graph shows that best fit straight line is not suited to lower values and upper values of turbidity.

Therefore other best fit lines have to be considered. Fig 4-2 shows the Logarithmic line. Non linear regression technique is also same as linear regression technique. There also correlation coefficient, r can take on values from 0 to 1, where 1 means there is a perfect match and means that all the points are on the line exactly.

According to the Fig 4-2,

• R-squared, r^2 = 0.4944

• Correlation Coefficient, r = 0.7031

Also the graph shows that best fit logarithmic line is not suited to lower values and upper values of turbidity.

Therefore other best fit lines have to be considered. Fig 4-3 shows the second order polynomial line.

According to the Fig 4-3,

• R-squared, $r^2 = 0.8573$

• Correlation Coefficient, r = 0.9259

According to the results correlation coefficient, r value is close to 1 and that indicated excellent second order polynomial reliability.

However other best fit lines are also considered. Fig 4-4 shows the power line.

According to the Fig 4-4,

• R-squared, r^2 = 0.6504

• Correlation Coefficient, r = 0.8064

The graph shows that best fit logarithmic line is not suited to upper values of turbidity.

Fig 4-5 shows the exponential line.

According to the Fig 4-5, University of Moratuwa, Sri La

• R-squared, r^2 w=w.110.810610.1k

• Correlation Coefficient, r = 0.9003

Therefore best suited curve fit is polynomial. However high order polynomial reliability is also considered. Fig 4-6 shows the third order polynomial line.

According to the Fig 4-6,

• R-squared, $r^2 = 0.8575$

• Correlation Coefficient, r = 0.9260

Fig 4-7 shows the fourth order polynomial line.

According to the Fig 4-7,

• R-squared, $r^2 = 0.8577$

• Correlation Coefficient, r = 0.9261

Fig 4-8 shows the fifth order polynomial line.

According to the Fig 4-8,

• R-squared, $r^2 = 0.861$

• Correlation Coefficient, r = 0.9279

Fig 4-9 shows the sixth order polynomial line.

According to the Fig 4-9,

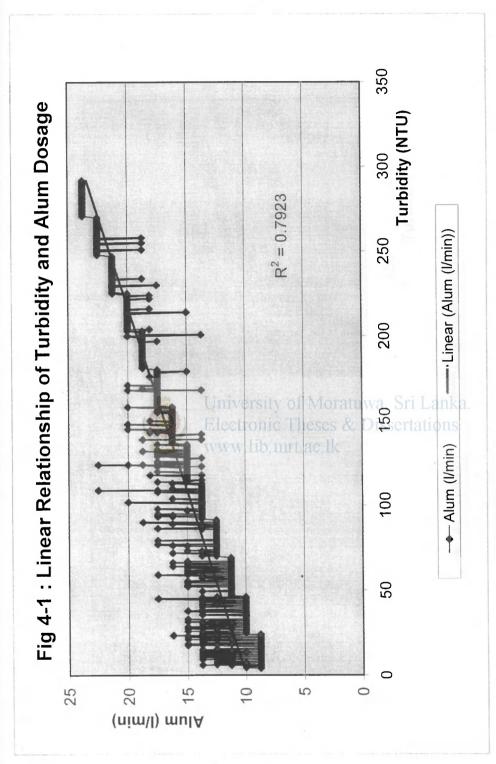
• R-squared, $r^2 = 0.8619$

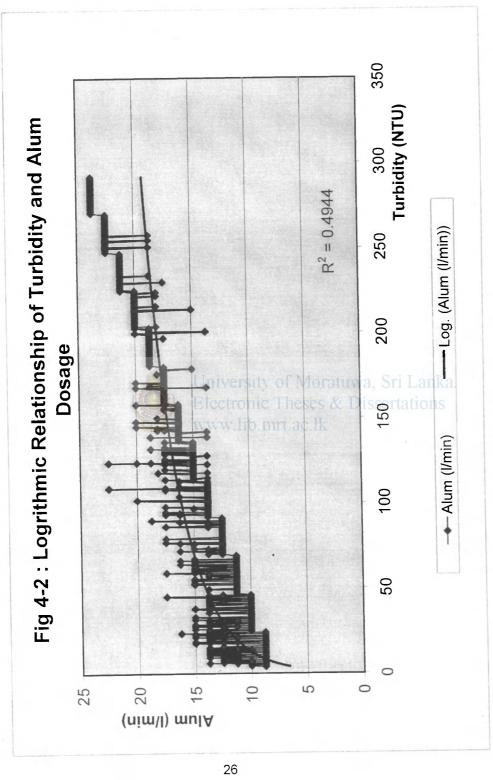
• Correlation Coefficient, r = 0.9283

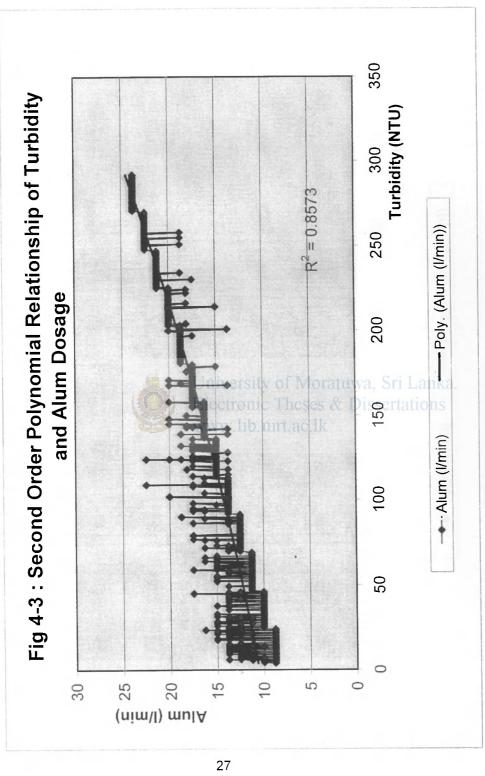
Table 4-1: Details of R-Squared Value with Different Lines

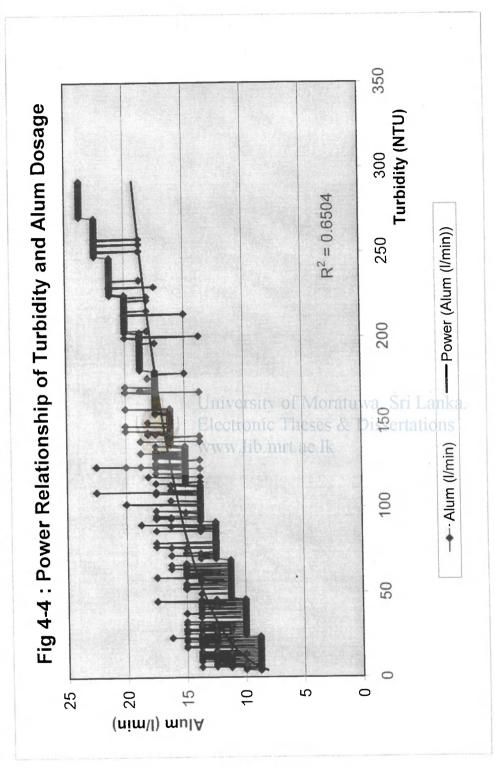
Ве	st fit	R-squared, r ²	Correlation Coefficient, r	1-r
1.	Straight line	0.7923	0.8901	0.1099
2.	Logarithmic line	0.4944	0.7031	0.2969
3.	Second Order Polynomial	0.8573	1110000 00 10100111111	ons 0.0741
4.	Third Order Polynomial	0.8575	0.9260	0.0740
5.	Fourth Order Polynomial	0.8577	0.9261	0.0739
6.	Fifth Order Polynomial	0.861	0.9279	0.0721
7.	Sixth Order Polynomial	0.8619	0.9283	0.0717

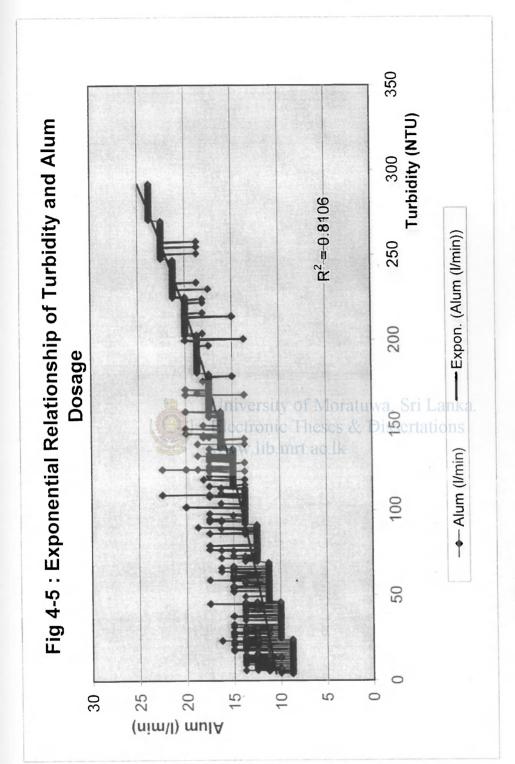
According to the table Correlation Coefficient, r is considerably near to 1 in polynomial line. Therefore this data is reliable for polynomial. And also it reveals that higher the order of the polynomial, better the curve fit. But Correlation Coefficient, r is changing considerably small. Therefore second order polynomial is reliable for data points.



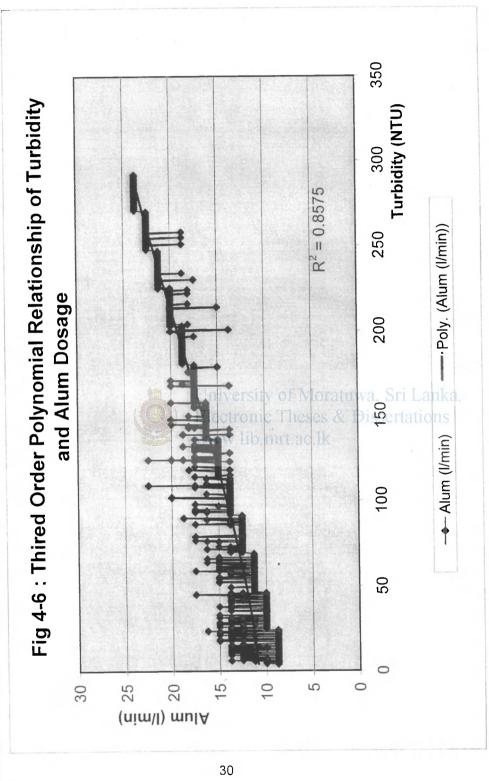


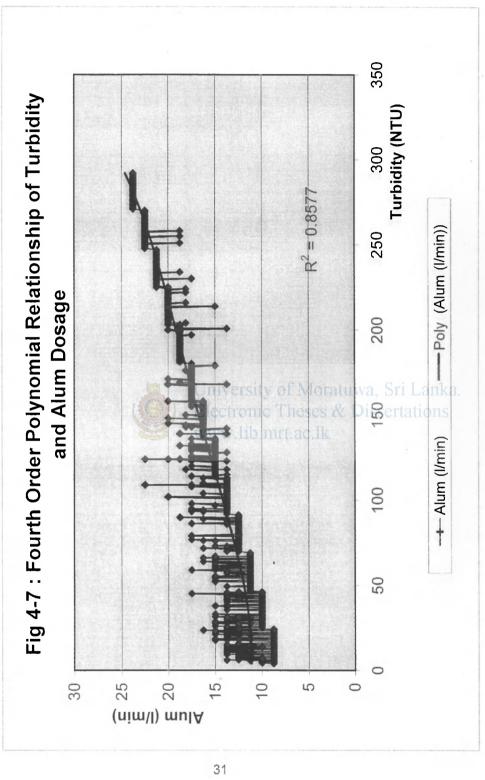


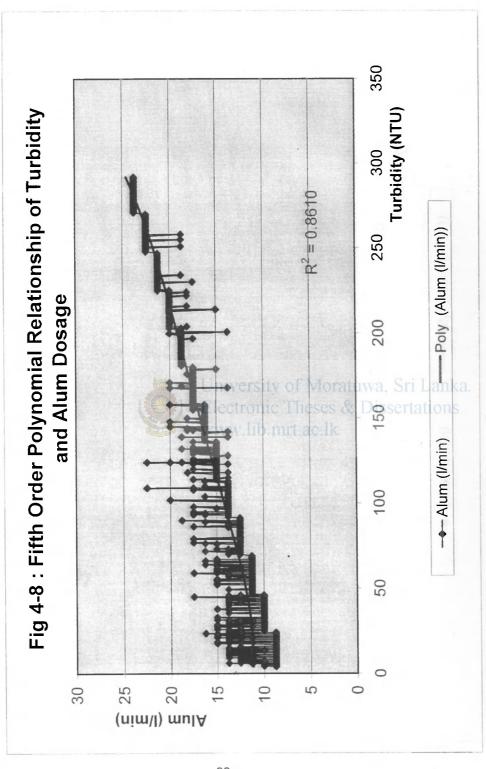


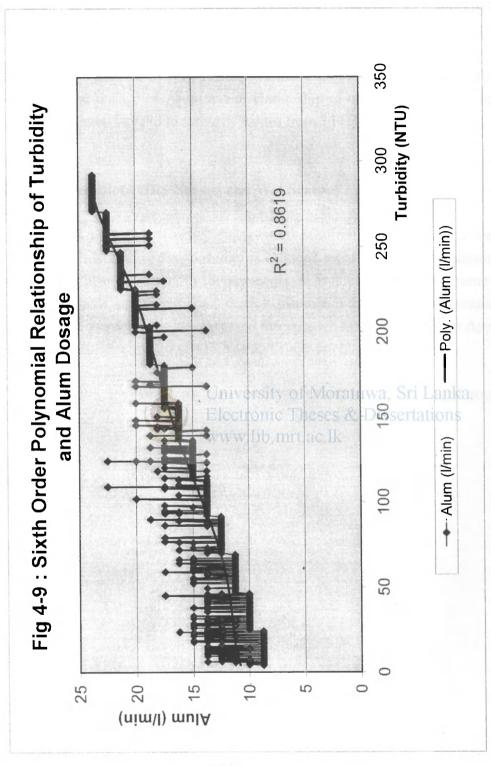












Relationship

OPTIMUM ALUM
$$= 10 + 0.05 \text{ (TURBIDITY)} + 6 \times 10^{-5} \text{ (TURBIDITY)}^2$$

DOSSAGE (l/min)

Turbidity is measured in NTUs. It shows that relationship of turbidity value of raw water and the dosage of Alum has a relationship of second order polynomial. And also this equation is valid to turbidity values from 2 NTU to 300 NTU.

Seasonal Variations (Dry Season and Wet Season)

In Sri Lanka only two seasonal changes are occurred, dry season and wet season. However if it is a rainy day, turbidity is changed rapidly both in wet season and dry season. And also according to the Appendix-A, it is observe that for same turbidity values has same optimum Alum dosage whether it belongs to dry season or wet season. For an example, it is considered the samples from 825 to 860 in Appendix-A. Then the season is checked and following details are obtained.

Therefore optimum dosage for same turbidity values may not changed according to the season.

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Table 4-2: Details of Seasonal Variations

Sample	Turbidity	Alum		Dry Season	Wet Season
No	(NTU)	(ppm)	Alum (l/min)		ASSEMBLE IN
825	204.0	16	20	√	
826	204.0	16	20		1
827	205.0	16	20	V	
828	205.0	16	20		√
829	206.0	16	20		V
830	206.0	16	20		V
831	207.0	16	20		V
832	207.0	16	20		√
833	208.0	16	20		
834	208.0	16	20		V
835	209.0	16	20		1
836	209.0	16	20	V	
837	209.0	16	20		V
838	210.0	16	20		V
839	210.0	16	20		V
840	211.0	16	20	V	
841	211.0	16	20	V	
842	212.0	16 Un	iversit20f Mor	atuwa, Sri L	anka. √
843	212.0	(16 Ele	ctroni20 heses	& Dissertati	ons √
844	213.0	16 ww	w.lib.20t.ac.lk		V
845	213.0	16	20		V
846	214.0	12	15	V	
847	214.0	16	20		V
848	214.0	16	20		V
849	215.0	16	20		√
850	215.0	16	20	V	
851	216.0	14.5	18.13		V
852	216.0	16	20		V
853	216.0	16	20		√ V
854	217.0	16	20		V
855	217.0	16	20		V
856	218.0	16	20	V	sam
857	218.0	16	20		1
858	219.0	16	20		√
859	219.0	16	20		√
860	220.0	16	20		V

Relationship of Lime dosage with pH value for LDC

After analyzing of turbidity of raw water and Alum dosage which is measured by Jar test from May, 2006 to April, 2007, Table 4-3 is obtained.

Table 4-3 Details of Experimental Lime Dosage for Different pH Values

pH Value	No of Samples			Lin	ne Dosa	nge (l/m	nin)		
	,	17.5	15	12.5	10	7.5	5	2.5	0
5.8	54	53		1					
5.9	54	1	52	1					
6.0	54	1	53						
6.1	56			56					
6.2	70		1	57	12				
6.3	77		4	8	65				
6.4	116	3	2	23	85	3			
6.5	147		l nivere	16	48	78	ri I anl	F.O.	4
6.6	101) F	lectror	ic 3 The	29	66	ttation	ka.	2
6.7	79	S W	ww lil	mrta	c lk	3	73		3
6.8	65					1	59	3	2
6.9	68					1	7	59	1
7.0	54				1				53
7.1	2								2
7.2	1								1
7.3	2			•					2

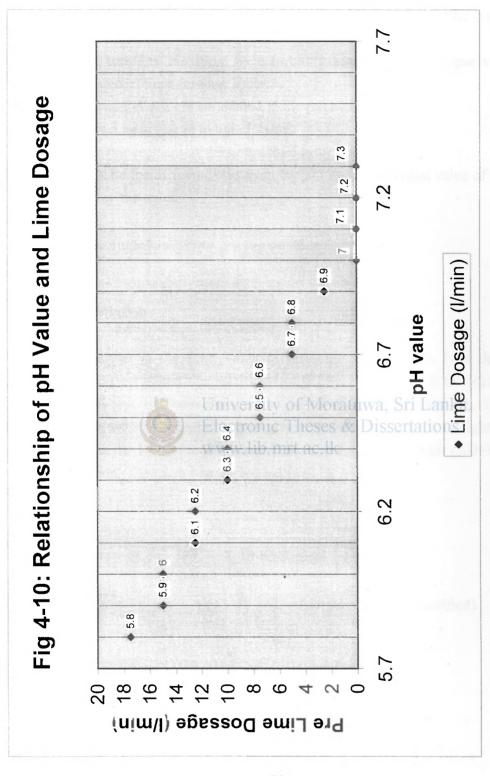
According to the Table 4-3, it shows that for all individual pH value has particular optimum Lime dosage which has occurred frequently. As an example, when pH value is equal to 6.3, optimum Lime dosage is 10 l/min in 65 times out of 77 samples. Therefore pH value of raw water and the optimum dosage of Lime have stepwise relationship.

Table 4-4 Requirement of Alum dosage for different pH values

pH value	Lime Dosage (l/min)	
5.8	17.5	
5.9	15.0	
6.0	15.0	
6.1	12.5	
6.2	12.5	
6.3	10.0	
6.4	10.0	
6.5	7.5	8
6.6	7.5	
6.7	5.0	9,
6.8	5.0	
6.9	2.5	3.0
7.0	University of Mo	ratuwa, Sri Lanka. & Dissertations
7.1	www0.0 mrt.ac.ll	
7.2	0.0	,
7.3	0.0	

Validity of the Equations

After obtaining optimum values for Alum and Lime dosage, they were applied to three hundred real situations. Then quality of final water was measured. According to the WHO (World Health Organization) Guide Lines, recommended value of turbidity is smaller than 5 and recommended pH value is smaller than 8. Those conditions are satisfied. Therefore relationships for optimum dosage of Alum and Lime are accurate.



4.3 Development of the system

The Fig 4-11, system diagram illustrates the basic structure used by the system.

The value of turbidity measured by a turbidity sensor is an analogue value that is given as an input to the microcontroller.

Following computations are conducted in the microcontroller.

- Convert analogue to a digital value.
- Make the decision of the optimum dosage value.
- Calculate the difference between current value and initial value of turbidity.
- Display the value

The above mentioned functions are explained with an example.

Sample Calculation

Let's assume that at the start, value of turbidity is 124 NTU. First that value is converted to digital value. The ADRESH:ADRESL register pair is the location where the 10-bit A/D result is loaded at the completion of the A/D conversion. This register pair is 16-bits wide. The A/D module gives the flexibility to left or right justify the 10-bit result in the 16-bit result register. The A/D Format Select bit (ADFM) controls this justification. The extra bits are loaded with '0' s.

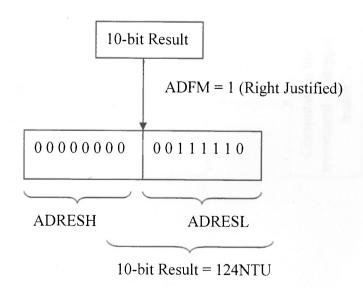




Fig 4-11 System Diagram

The data base is developed to find the optimum Alum dosage (Refer Appendix-D). It is based on the equation obtained between the value of turbidity and the optimum alum dosage (Optimum Alum Dosage = $10 + 0.05 \times (Turbidity) + 6 \times 10^{-5} \times (Turbidity)^2$).

According to the field data turbidity varies from 4 NTU to 292 NTU. Therefore half step mode permanent magnet stepper motor with 1.8° step angle is used. In Appendix-D, angle movement of stepper motor for different turbidity values is also shown. Then the criterion is defined to select the angle movement of stepper motor with digital value of turbidity in the source code (Appendix-C).

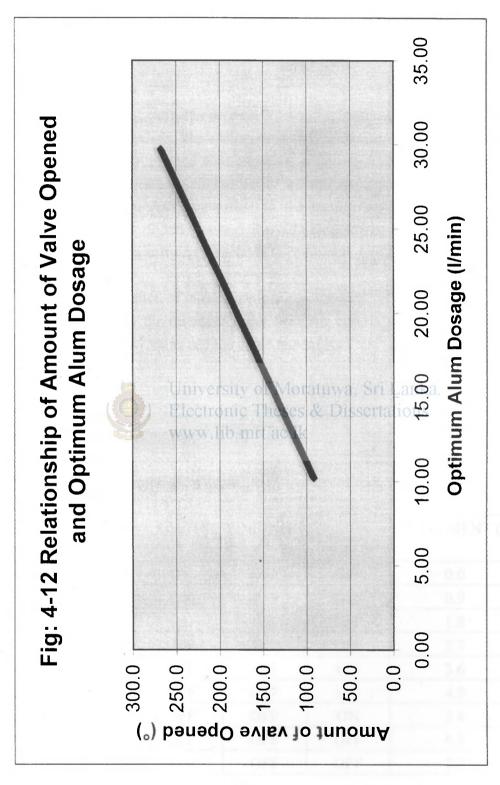
As per the example, angle movement of the stepper motor is 154.1°. Since the optimum Alum dosage is proportional to the angle movement of stepper motor, optimum Alum dosage is also proportional to amount of valve opened. Figure 4-12 shows the relationship of amount of valve opened and optimum Alum dosage.

Then also a loop is defined to giving interrupts when turbidity value is changed by 10.

Initial value - 124NTU - '0000111110' Saturation value - 134NTU - '0010000110'

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Then the flag is on and change the angle accordingly. Movement of the angle for 134NTU is 160°.



Design of the hardware

The Fig 4-12, shows the Schematic Diagram of the Hardware used by the system.

Following major components are indicated in the diagram.

• A/D converters

The Analog to digital converter module has five inputs for the 28 pin devices and eight for the other devices. The analog input charges a sample and hold capacitor. The output of the sample and hold capacitor is the input into the converter. The converter then generates a digital result of this analog level via successive approximation. The A/D conversion of the analog input signal results in a corresponding 10 bit digital number. The A/D module has high and low voltage reference input that is software selectable to combination of RA2 and RA3.

- Selection and calculation of motor position
 Selection is done by the microcontroller from the criteria written with referring
 Appendix-D, turbidity value and the angle movement.
- Stepper motor controlling University of Moratuwa, Sri Lanka.
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 Table 4-5 shows the sequence. Lib. mrt. ac.lk

Table 4-5: The sequence of switching the windings of ADC

STEP		STATOR '	MOVEMENT (°)		
	1	2	3	re pir4 data	in, clock, and toad.
0	ON	ON	OFF	OFF	0.0
0.5	OFF	ON	OFF	OFF	0.9
1	OFF	ON	ON	OFF	1.8
1.5	OFF	OFF	ON	OFF	2.7
2	OFF	OFF	ON	ON	3.6
2.5	OFF	OFF	OFF	ON	4.5
3	ON	OFF	OFF	ON	5.4
3.5	ON	OFF	OFF	OFF	6.3
4	ON	ON	OFF	OFF	7.2

Either increment or decrement of the value of pH value by 0.1 makes the changing of valve position in LDC. Alum is changed from 5.5 to 7.5. Full step mode permanent magnet stepper motor with 15° step angle is used. Table 4-6 shows the sequence.

Table 4-6: The sequence of switching the windings of LDC

STEP		STATOR '	WINDING		MOVEMENT (°)
	1	2	4		
0	ON	ON	OFF	OFF	0
1	OFF	ON	ON	OFF	15
2	OFF	OFF	ON	ON	30
3	ON	OFF	OFF	ON	45
4	ON	ON	OFF	OFF	60

• Display unit using MAX7219

The MAX7219 drives common-cathode LED displays from one to eight seven-segment digits in length. It can also be used to drive up to 64 discrete LEDs configured as eight common-cathode clusters of eight LEDs each.

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When the MAX7219 is used with seven-segment displays, it can be configured to automatically convert binary-coded decimal (BCD) values into appropriate patterns of segments.

The MAX7219 interfaces with controllers through three pins: data in, clock, and load. It connects to the LED displays in a straightforward way; pins SEG A through SEG G and SEG DP connect to segments A through G and the decimal point of all of the common-cathode displays. Pins DIGIT 0 through DIGIT 7 connect to the individual cathodes of each of the displays.

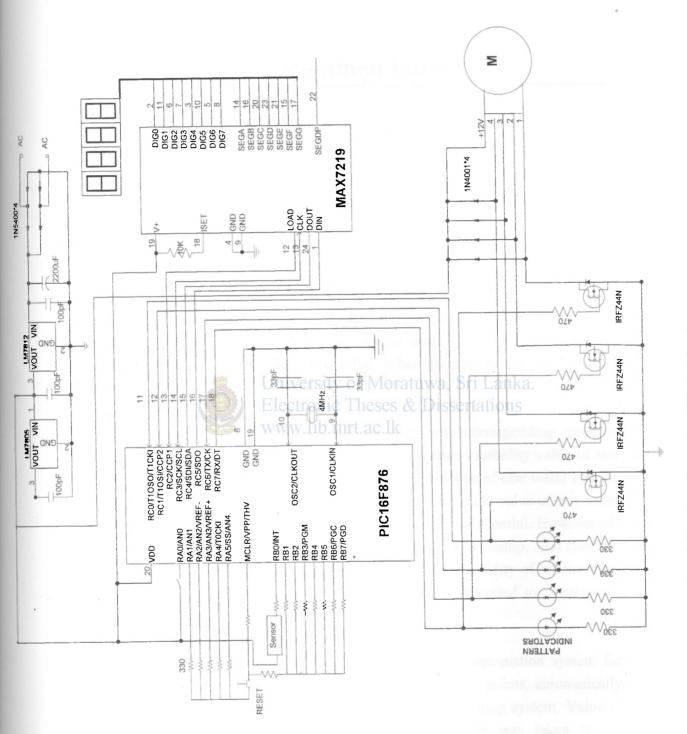


Fig 4-12: Schematic Diagram of the Hardware

Chapter 5

Conclusions and Recommendations

5.1 Conclusions, Remarks and Discussion

To conclude, this research adhered to the initial objectives, which were stated. The major activity of this research was to propose an alternative to the jar test allowing for an on line determination of optimal coagulant dosage from raw water characteristics and design a system for feeding Alum and Lime automatically with a monitoring display.

Coagulant dosing rate is non-linearly correlated to raw water parameters of turbidity, conductivity, pH, temperature, dissolved oxygen and UV's absorption. It was assumed that except turbidity and pH value, other parameters are almost same throughout year.

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After analyzing thousand number of jar test results with corresponding turbidity values and pH value of incoming water, it was demonstrated turbidity value of raw water and the dosage of Alum has a relationship and pH value of raw water and the dosage of Lime has another relationship. Relationship of turbidity value of raw water and the dosage of Alum has a relationship of second order polynomial. However pH value of raw water and the dosage of Lime have stepwise relationship. And also real three hundred situations were taken and applied to check the validity of relationships and it proved that relationship which has obtained are well suited to develop the automation system.

The major component of the research is designing a fully automation system for measuring the turbidity and pH value, deciding the operating points, automatically changing the dosage accordingly and turbidity and pH monitoring system. Value of turbidity was measured by a turbidity sensor. That value was taken to the microcontroller and it decided the Alum dosage and changes the valve position using stepper motor accordingly. Either increment or decrement of the value of turbidity by

10 makes the changing of valve position in ADC. Either increment or decrement of the value of pH value by 0.1 makes the changing of valve position in LDC. Using MAX7219 IC value of current value of turbidity and current value of pH are displayed in ADC and LDC respectively.

System consists three major parts. They are sensors (turbidity sensor for ADC and pH sensor for LDC), controller and stepper motor. Selected turbidity meter, WQ710 was perfectly matched for the design since it can be inserted into low pressure pipes by using standard compression coupler for turbidity monitoring and readings are giving every three seconds. It showed that output currents at the maximum turbidity values close to 20mA, so that it is easy to work with microcontroller.

PIC16F876 microcontroller is selected as the controller; it made the task easier. Since PIC16F876 has 8-bit with analogue to digital converters it handled analogue output of turbidity sensor and pH sensor. In this project MAX 7219 display driver IC could be easily interfaced with microcontroller by using three wires (SDO, SDI and SCLK) and LOAD (CE) which is common today named as Serial Peripheral Interface (SPI). The PIC16F876 chip is in electrical erasable packaged version (FLASH), and it helped for programming several times for testing our objective is implemented. PIC16F876 was simple for motor controlling specially stepper motor controlling.

The varieties of software tools are available for developing and debugging source code for the controller. The MPLAB software is used for developing the system which is windows based an easy software development in 8-bit microcontroller and it made developing and debugging the source code easy and simple.

5.1 Recommendations for Future Research

The recommendations given in this chapter is mainly based on the research findings.

All this research shows that any complex situation can be handled by doing reasonable assumptions and using simple selections. Tropical countries like Sri Lanka can use this simplification method for different lakes and rivers. After analyzing a water source, relationships for Alum and Lime dosing with turbidity and pH value can be found. For Kelani River relationship of turbidity value of raw water and the dosage of Alum has a relationship of second order polynomial and pH value of raw water and the dosage of Lime have stepwise relationship.

Since such relationship is found controlling part became easier and low cost. The main controller, which is PIC16F876, handled A/D converting and stepper motor controlling perfectly. And also MAX 7219 display driver IC is easily interfaced with microcontroller. The MPLAB software is used for developing the system has developed and debugged the source code easily.

Considering the practical situation constructing such equipment is low cost. And also it can decrease operational cost, chemical cost, laboratory tests and unnecessary manhours.



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Appendices

Appendix A - Jar Test Results and Calculated Values of Dosages in the Field

Appendix B - Final Water Quality for Constructed values of Optimum Values of dosing

Appendix C - Development of the Source Code

Appendix D - Data base for Turbidity, Optimum Dosage and Angle Movement of Stepper Motor



Appendix-A

Appenaix							1	
Sample			Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(l/min)
1	4.0	5.8	7	17.5	5	12.5	7	8.75
2	4.0	6.1	5	12.5	5	12.5	7	8.75
3	4.0	6.4	4	10	5	12.5	7	8.75
4	4.4	7	0	0	5	12.5	8	10
5	4.92	6.5	3	7.5	5	12.5	8	
6	5.0	5.9	6	15	6	15	7	8.75
7	5.0	6.2	5	12.5	5	12.5	7	8.75
8	5.0	6.5	3	7.5	5	12.5	7	8.75
9	5.3	6.8	0	0	5	12.5	8	10
10	5.4	6.7	3	7.5	5	12.5	8	10
11	5.66	6.7	0	0	5	12.5	7	8.75
12	5.7	7.3	2	5	5	12.5	9	11.25
13	5.8	6.5	3	7.5	5	12.5	9	11.25
14	5.93	6.6	3	7.5	5	12.5	11	13.75
15	6	6.8	4	10	6	15	9	11.25
16	6.0	6	6	15	6	15	7	8.75
17	6.0	6.3	4	10	5	12.5	7	8.75
18	6.0	6.6	3	7.5	5	12.5	7	8.75
19	6.1	6.6	0	0	5	12.5	8	10
20	6.2	6.4	3	7.5	Jaratuw 5	12.5	10	12.5
21	6.2	6.6	3	7.5	101 atuwa 5	12.5	8	10
22	6.3	6.5	Elegi	7.5	ses & Dis	12.5	10	12.5
23	6.4	6.6	WW3	.l1b.m17.5	5. <u>lk</u> 5	12.5	8	10
24	6.4	6.6	3	7.5	5	12.5	8	10
25	6.5	6.5	3	7.5	5	12.5	10	12.5
26	6.5	6.5	3	7.5	5	12.5	10	12.5
27	6.6	6.6	3	7.5	5	12.5	9	11.25
28	6.8	7.1	0	0	5	12.5	8	10
29	6.8		3	7.5		12.5	10	12.5
30	6.9	6.5	3	7.5	5	12.5	8	10
31	6.9	6.6	3	7.5	5	12.5	10	12.5
32	6.9	6.7	0	0	5	12.5	8	10
33	6.9	6.6	0	0	5	12.5	8	10
34	7	6.9	0	0	6	15	9	11.25
35	7	6.6	3	7.5	5	12.5	10	12.5
36	7	6.6	3	7.5	5	12.5	8	10
37	7.0	6.1	5	12.5	6	15	7	8.75
38	7.0	6.4	4	10	5	12.5	7	8.75
39	7.0	6.7	2	5	5	12.5	7	8.75
40	7.11	6.7	3	7.5	5	12.5	10	12.5
41	7.2	6.9	3	7.5	5	12.5	10	12.5
42	7.3		3	7.5	5	12.5	8	10
43	7.3	6.5	0	0	5	12.5	8	10



Sample	mg 1 2 2 2 4 4		1	Pre Lime	Post Lime (ppm)	Post Lime	Alum (ppm)	Alum (l/min)
	Turbidity	pH	(ppm)			12.5	10	12.5
44	7.3	6.9					10	12.5
45	7.3	6.9					10	12.5
46	7.3	6.9					-	12.5
47	7.3	6.9					-	11.25
48		-		7.5			10	12.5
49		-		3 7.5			10	12.5
50	7.5	-		3 7.5		12.5	10	12.5
51		_		3 7.5		12.5	5 10	
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54		_		3 7.		12.5	5 10	
55						3 15	5 9	1
56		-		3 7.	5 5	5 12.5		
57		-		3 7.	5	5 12.		
58		-	_	3 7.	5	5 12.		_
59		_		3 7.	5	5 12.		_
60		_		3 7.	5	5 12.	_	9 11.25
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		.0 6	5.5		.5	5 12		7 8.7
7	0 8	.0 6	5.8	-	5	5 12		7 8.7 9 11.2
7	1 8	.1 6	5.5		7.5	5 12		9 11.2
7	2 8	.1 6	6.4		10		5	
7	73 8		3.5		² .5		2.51	9 11.2 101 12
7			6.5		7.5			101 12
		_	5.5	4	10			9) 11.2
		_	3.5		7.5		2.5 <u> </u> 2.5	9 11.2
		_	3.5		7.5	_		10 12
	78	\rightarrow	6.5		7.5		7.5	7 8.
		-	6.3	4	10		2.5	7 8.
		_	6.6		7.5	_	2.5	7 8.
			6.9		2.5		2.5	9 11.
		_	6.5	4	10	0	0	111 13.
		_	6.5	4	10	4	101	101 12
		_	6.9	3	7.5	6	15	91 11.
		9.9	6.4	4	10		2.5	10 1
	86 9	.98	6.4	4	10	וו	2.01	101 1

Sample No	Turbidity	На	Pre Lime	Pre Lime (I/min)	Post Lime (ppm)	Post Lime (I/min)		Alum (I/min)
87	10.0	6.4		10	4	10	7	8.75
88	10.0	6.7		5	5	12.5	7	8.75
89	10.0	7	-	0	5	12.5	7	8.75
90	10.3	-			5		11	13.75
91	10.4	_		10	5		9	11.25
92	10.5	_		10	5	12.5		12.5
93	10.5	-		5	5			11.25
94		-			5	12.5		11.25
95		_			0	0	11	13.75
96		-			5	12.5	9	11.25
97		_			5 5	12.5	9	11.25
98	-	-		7.5		12.5	7	8.75
99		-		1 2.5		12.5	7	8.75
100		_		7 17.5		12.5	7	8.75
100		_	-	1 10		12.5	11	13.75
102		_	-	4 1		12.5	5 11	13.75
102	-	_	-	3 7.		4 10	10	12.5
		-	-	3 7.		5 12.	5 9	11.25
104				4 1		4 10	11	1 13.75
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11			.4		10		0 1	1 13.7
11			5.3	5 12		5 12		1 13.7
11		_	5.5		5	7 17		7 8.7
11		_	5.7		0	5 12		7 8.7
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			6.4	4	10		2.5	9 11.2
		_	6.5		7.5		2.5	9 11.2
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1		_	6.6		7.5			7 8.
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		4.0	5.8	7 1	7.5	5 12	2.5	/ 0.

Sample			Pre Lime	Pre Lime	Post Lime		Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(l/min)
130	14.0	6.1	5	12.5	5	12.5	7	8.75
131	14.3	6.4	4	10	0	0	11	13.75
132	14.5	6.4	4	10	5	12.5	9	11.25
133	14.5	6.4	5	12.5	6	15	10	12.5
134	14.8	6.6	4	10	5	12.5	11	13.75
135	15.0	6.9	1	2.5	7	17.5	7	8.75
136	15.0	5.9	6	15	5	12.5	7	8.75
137	15.0	6.2	5	12.5		12.5	7	8.75
138	15.1	6.2	5	12.5		12.5	10	12.5
139	15.1	6.4	4	10		12.5	11	13.75
140	15.1	6.6	4	10	5	12.5	10	12.5
141	15.3	6.8	3	7.5			10	12.5
142	15.3	6.6	3	7.5	5	12.5	10	12.5
143	15.6	6.2	5	12.5	5	12.5	10	12.5
144	16.0	7	0	0	5	12.5		8.75
145	16.0	6	6	15	5	12.5	7	8.75
146		6.3	4	10	5	12.5		8.75
147		5.8	7	17.5	6	15	7	8.75
148		6.1	5	12.5			7	8.75
149				1.0	5	12.5	7	8.75
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153		5.9			7	17.5	7	8.75
154		_		12.5	5	12.5	5 7	8.75
155		-				12.5	5 7	8.75
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162		_		1 10) !	5 12.	5 11	1 13.75
163		_		1 10		5 12.	5 1	1 13.75
164				5 12.5		5 12.	5 7	8.75
165		_		4 10		3 1:	5 7	8.75
166						5 12.	5 7	8.75
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21.2	0.0		-	10	5		12.5	9	11	1.25
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	-		4	10	5		12.5	11	_	3.75
21.4	-		4	10	5		12.5	10	_	12.5
22.0	-		4	10	5		12.5	7	_	8.75
	-	-	-	7.5	5		12.5	7	7	8.75
	-		_		5	5	12.5	7	7	8.75
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	-		_			5	12.5	5	7	8.75
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	$\overline{}$							15	7	8.7
_	_		-				12	2.5	7	8.7
			_				12	2.5	7	8.7
	-		\rightarrow					15	10	12.
	_		_				12	2.5	111	13.7
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Comple			Pre Lime	IP	re Lime	Post Lime	Po	st Lime			
Sample	Turbidity	рН	(ppm)	1		(ppm)	(1/	min)	(ppm)	(l/n	nin)
No	25.4	6.6		_	10	5	1	12.5	11	13	3.75
216	25.4	6.6	1	_	10	5	_	12.5	11	1:	3.75
217	25.7	6.1		-	12.5	8	_	20	12		15
218		_		5	12.5	6		15	10		12.5
219 220		-		2	5	6		15	8		10
220	26.0	-	-	0	0	5	5	12.5		_	10
222		-		6	15	5	5	12.5		_	10
223		-		1	2.5	6	3	15		_	10
224		-		7	17.5		5	12.5		+	10
225		-		5	12.5		5	12.5		-	10
226		_		5	12.5		3	15		_	12.5
227				4	10		5	12.5		_	15
228		_		4	10		5	12.5		_	1.25
229		_		4	10			(_	15
230		-		1	v of \2.	5 caturna 6	5	12.5		В	10
23				6	1	0.00	4	Lailkq		8	10
23				5	12.	5 & Disse	6	ations 1		8	10
23				4	mrt.ac1		5	12.		_	13.75
23		_	.7	4	1	0	5	12.		_	13.75
23	•	_	.3	5	12.	5	5	12.		2	15
23		_	7	0		0	6			8	10
23	_		6	6		5	6			8	10
23		0 6	.3	4		0	6		5	8	10
23		6 6	.7	4		0	5	12.	_	_	13.75
24		.0 5	.8	7	17		6		5	8	10
24		.0 6	1.1	5	12		6		5	8	10
24		.0 6	5.4	4		0	6		5	8	13.75
24			7	4		0	5	12	-	1C	12.5
24	14 30	.7 6	5.5	4		10	5	12		91	11.25
			3.3	5			5		.51	101	12.5
24	46	_	3.3	5		.5	5		5l 5l	91	11.25
24	47		5.3	4	-	10	5		51 15l	81	10
2	48 31		5.9	1		151	6		15	131	10
2	49 31	_	6.2			5	3		15	31	10
2			6.5			7.5	5		2.5	111	13.75
2	51 31		6.3	_		10			15	121	15.75
2	52 31	1.4	6.3			2.5	6		15	BI	10
2		2.0	6	_	3	15	6		2.5	BI	10
2		_	6.3	_	41	10	5		2.5	8	10
2		_	6.6	_		7.5	<u>5</u>		15	12	15
2		-	6.3	_		2.5			15	8	10
2		_	6.1			2.5	6		15	81	
2	258 3	3.0	6.4		4	10)	101	- 0	

Sample		l	Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(I/min)
259	33.0	6.7	2	5	6	15	8	. 10
260	34.0	6.2	5	12.5	6	15	8	10
261	34.0	6.5	3	7.5	6	15	8	10
262	34.0	6.8	1	2.5	6	15	8	10
263	35.0	6.3	4	10	6	15	8	10
264	35.0	6.6	3	7.5	6	15	8	10
265	35.0	6.9	1	2.5	6	15	8	10
266	35.5	6.5	4	10	5	12.5	11	13.75
267	36.0	6.4	4	10	6	15	8	10
268	36.0	6.7	2	5	6	15	8	10
269	36.0	7	0	0	6	15	8	10
270	37.0	6.5	3	7.5	6	15	8	10
271	37.0	6.8	1	2.5	5	12.5	8	10
272	37.0	5.8	7	17.5	7	17.5	8	10
273	37.2	6.5	4	10	5	12.5	11	13.75
274	37.4	6.5	4	10	5	12.5	11	13.75
275	37.8	6.6	5	12.5	5	12.5	12	15
276	38.0	6.6	3	7.5	6	15	8	10
277	38.0	6.9	1	2.5	5	12.5	8	10
278	38.0	5.9	6	15	4	10	8	10
279	38.5	6.5	Uni.4	reity of 10	oratuwa 5	i Lank 12.5	11	13.75
280	39.0	6.7	_ 2	The 5	& Dicco	tations 15	8	10
281	39.0	7	0	0	6	15	8	10
282	39.0	6	WW 6	15	5	12.5	8	10
283	40.0	6.8	1	2.5	6	15	8	10
284	40.0	5.8	7	17.5	6	15	8	10
285	40.0	6.1	5	12.5	6	15	8	10
286	40.1	6.5	4	10	5	12.5	11	13.75
287	41.0	6.9	1	2.5	6	15	8	10
288	41.0	5.9	6	15	6	15	8	10
289	41.0	6.2	5	• 12.5	7	17.5	8	10
290	41.2	6.5	4	10	5	12.5	11	13.75
291	41.4	6.5	4	10	5	12.5	11	13.75
292	41.7	6.8	3	7.5	5	12.5	10	12.5
293	41.9	6.7	4	10	5	12.5	11	13.75
294	42.0	7	0	0	6	15	8	10
295	42.0	6	. 6	15	5	12.5	8	10
296	42.0	6.3	4	10	7	17.5	8	10
297	43.0	6.5	4	10	5	12.5	11	13.75
298	43.0	5.8	7	17.5	6	15	8	10
299	43.0	6.1	5	12.5	5	12.5	8	10
300	43.0	6.4	4	10	7	17.5	8	10
301	43.7	6.5	4	10	5	12.5	11	13.75

Sample			Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Aluma
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(I/min)	(ppm)	Alum (I/min)
302	44.0	5.9	6	15	6	15	(PPIII)	
303	44.0	6.2	5	12.5	5	12.5	8	
304	44.0	6.5	3	7.5	5	12.5	8	
305	45	6.5	5	12.5	6	15		-
306	45.0	6	6	15	6	15		
307	45.0	6.3	4	10	5	12.5		
308	45.0	6.6	3	7.5	6	15	8	10
309	45.8	6.5	4	10	5	12.5	11	13.75
310	46	6.5	5	12.5	5	12.5	10	12.5
311	46.0	6.1	5	12.5	6	15	8	10
312	46.0	6.4	4	10	5	12.5	8	10
313	46.0	6.7	2	5	7	17.5	8	10
314	47.0	6.2	5	12.5	6	15		11.25
315	47.0	6.5	3	7.5	5	12.5	9	11.25
316	47.0	6.8	1	2.5	6	15		11.25
317	48.0	6.3	4	10	6	15		11.25
318	48.0	6.6	3	7.5	5	12.5		
319	48.0	6.9	1	2.5	5	12.5		11.25
320	49.0	6.4	4	10	6	15		
321	49.0	6.7	2	5	5	12.5		
322	49.0	7	Univ0	sity of M	oratuwa, 5	i Lank 12.5	9	-
323	49.3	6.5	Elect ⁴	onic The 10	s & Disso	tations 12.5	11	
324	50.0	6.5	3	7.5	6	15		
325	50.0	6.8	1	2.5	6	15		
326	50.0	5.8	7	17.5	5	12.5	9	
327	51.0	6.6	3	7.5	6	15	9	
328	51.0	6.9	1	2.5	6	15		-
329	51.0	5.9	6	15	6	15	9	
330	52.0		2	5		15		
331	52.0	7	0	0	6	15		
332	52.0	6	6	15	6	15		
333	52.1 52.4	6.6	4	10	5	12.5		15
334 335		6.6	4	10	5	12.5	12	
336	52.8		4	10	5	12.5	12	15
337	53.0 53.0	6.8 5.8	1	2.5	6	15	9	
338	53.0	6.1	7	17.5	6	15	9	
339	54.0	6.9	5	12.5	7	17.5	9	
340	54.0	5.9	1 6	2.5	6	15	9	11.25
341	54.0	6.2	5	15	6	15	9	11.25
341	54.0	6.6	4	12.5 10	6	15	9	11.25
343	54.2	6.6	4		5	12.5	12	15
344	55.0	6.6	4	10 10	5 5	12.5 12.5	12 12	15 15

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime (I/min)	Alum (ppm)	Alum (l/min)
345	55.0	7	0	0	6	15	9	11.25
346	55.0	6	6	15	6	15	9	11.25
347	55.0	6.3	4	10	6	15	9	11.25
348	55.4	6.5	4	10	5	12.5	12	15
349	56.0	5.8	7	17.5	7	17.5	9	11.25
350	56.0	6.1	5	12.5	6	15	9	11.25
351	56.0	6.4	4	10	5	12.5	9	11.25
352	57.0	6.5	4	10	5	12.5	11	13.75
353	57.0	5.9	6	15	6	15	9	11.25
354	57.0	6.2	5	12.5	6	15	9	11.25
355	57.0	6.5	3	7.5	6	15	9	11.25
356	57.3	6.8	4	10	5	12.5	11	13.75
357	58.0	6	6	15	6	15	9	11.25
358	58.0	6.3	4	10	6	15	9	11.25
359		6.6	3	7.5	6	15	9	11.25
360		6.7	4	10	5	12.5	11	13.75
361	59	6.1	5	12.5	0	0	14	17.5
362		-	5		5	12.5	9	11.25
363						15	9	11.25
364		_				15	9	11.25
365			-	-		Sri I 212.5	12	15
366		-			THE RESERVE OF THE PARTY OF THE		12	15
367		-			7.0	17.5	18.0	22.5
368		-	WW	17.5	7.0	17.5	18.0	22.5
369		-		17.5	7.0	17.5	18.0	22.5
370		-		12.5	5 5	12.5	5 9	11.25
371			3	7.5	5 5	12.5	5 9	11.25
372		+		2.5			5 9	11.25
373		-				12.5	5 12	15
374		_		10	5	12.5	5 9	11.25
375		-		7.5	5 5	12.5	5 9	11.25
376		_		2.5				
377		_				15	5 12	2 15
378		_		1 10			5 9	11.25
379		_			5 5		5 9	11.25
380								11.25
381		_		7 17.5				
382				3 7.5	5 !	12.		11.25
383		_		1 2.5	5 5	12.		11.25
384		_		7 17.		1:		11.25
385		_		7 17.			_	
386				3 7.		1:		11.25
387		_		1 2.		12.		11.25

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime	Alum (ppm)	Alum (I/min)
388	64.0	5.9	6	15	6	15	9	
389	65.0	6.7	2	5	6	15	9	11.25
390	65.0	7	0	0	5	12.5	9	11.25
391	65.0	6	6	15	6	15	9	11.25
392	65.1	6.6	4	10	5	12.5	12	15
393	66.0	6.8	1	2.5	6	15	9	11.25
394	66.0	5.8	7	17.5	5	12.5	9	11.25
395	66.0	6.1	5	12.5	6	15	9	11.25
396	66.1	6.6	4	10	6.0	15	13.0	16.25
397	66.4	6.5	4	10	5	12.5	12	15
398	67.0	6.3	7	17.5	7.0	17.5	18.0	22.5
399	67.0	6.9	1	2.5	7	17.5	9	11.25
400	67.0	5.9	6	15	5	12.5	9	11.25
401	67.0	6.2	5	12.5	6	15	9	11.25
	68.0	7	0	0	7	17.5	9	11.25
403	68.0	6	6	15	5	12.5	9	11.25
404	68.0	6.3	4	10	6	15	9	11.25
406	69.0 69.0	5.8	7	17.5	5	12.5	9	11.25
407	69.0	6.4	5	12.5	5	12.5	9	11.25
408	70.0	5.9	4	10	6	15	9	11.25
409	70.0	6.2	Univer6	ty of Mt5	atuwa, Sr 5	_anka.12.5	10	12.5
410	70.0	6.5	Flectro ⁵	ic Thd2.5	& Disser5	ions 12.5	10	12.5
411	70.1	6.4	www.13	mrt.a.7.5	6	15	10	12.5
412	71.0	6	6	7.5	5	12.5	11	13.75
413	71.0	6.3	4	15 10	6	15	10	12.5
414	71.0	6.6	3		5	12.5	10	12.5
415	71.9	6.4	6	7.5	6	15	10	12.5
416	72.0	6.1	5	12.5	7	17.5	13	16.25
417	72.0	6.4	4	10	6	15	10	12.5
418	72.0	6.7	2	5	6	12.5	10	12.5
419	73.0	6.3	7	17.5	7.0	15	10	12.5
420	73.0	6.2	5	12.5	6	17.5	18.0	22.5
421	73.0	6.5	3	7.5	5	15	10	12.5
422	73.0	6.8	1	2.5	6	12.5 15	10	12.5
423	73.2	6.6	4	10	5	12.5	10	12.5
424	74.0	6.3	4	10	5	12.5	12	15
425	74.0	6.6	3	7.5	5	12.5	10	12.5
426	74.0	6.9	1	2.5	6	15	10	12.5
427	75.0	6.4	4	10	6	15	10	12.5
428	75.0	6.7	2	5	5	12.5	10	12.5 12.5
429	75.0	7	0	0	6	15	10	12.5
430	76.0	6.5	3	7.5	6	15	10	12.5

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime	Alum (ppm)	Alum (I/min)
431	76.0	6.8	1	2.5	5	12.5	10	12.5
432	76.0	5.8	7	17.5	. 6	15	10	12.5
433	76.1	6.5	4	10	5	12.5	12	15
434	76.4	6.6	4	10	5	12.5	13	16.25
435	77	6	7	17.5	7	17.5	14	17.5
436	77.0	6.5	5	12.5	6	15	10	12.5
437	77.0	6.6	3	7.5	0	0	10	12.5
438	77.0	6.9	1	2.5	6	15	10	12.5
439	77.0	5.9	6	15	6	15	10	12.5
440	78.0	6.7	2	5	6	15	10	12.5
441	78.0	7	0	0	6	15	10	12.5
442	78.0	6	6	15	6	15	10	12.5
443	79.0	6.8	1	2.5	6	15	10	12.5
444	79.0	5.8	7	17.5	6	15	10	12.5
445	79.0	6.1	5	12.5	6	15	10	12.5
446	79.2	6.5	4	10	5	12.5	14	17.5
447	80.0	6.9	1	2.5	7	17.5	10	12.5
448	80.0	5.9	6	15	7	17.5	10	12.5
449	80.0	6.2	5	12.5	6	15	10	12.5
450	80.2	6.5	5	12.5	6	15	10	12.5
451	81.0	7	I Inive 0	ity of MO	ratuwa S5	Lanka12.5	10	12.5
452	81.0	6	Flootr6	ric The 15	& Dissel	tions 20	10	12.5
453	81.0	6.3	4	10	6	15	10	12.5
454	82.0	5.8	WWW.7	17.5	6	15	10	12.5
455	82.0	6.1	5	12.5	5	12.5	10	12.5
456	82.0	6.4	4	10	6	15	10	12.5
457	83.0	5.9	6	15	6	15	10	12.5
458	83.0	6.2	5	12.5	4	10	10	12.5
459	83.0	6.5	3	7.5	6	15	10	12.5
460	84.0	6	6	.15	5	12.5	10	12.5
461	84.0	6.3	4	10	5	12.5	10	12.5
462	84.0	6.6	3	7.5	7	17.5	10	12.5
463	85.0	6.1	5	12.5	7	17.5	10	12.5
464	85.0	6.4	4	10	5	12.5	10	12.5
465	85.0	6.7	2	5	6	15	10	12.5
466	85.7	6.5	5	12.5	6	15	10	12.5
467	86.0	6.3	7	17.5	7.0	17.5	18.0	22.5
468	86.0	6.2	5	12.5	5	12.5	10.0	12.5
469	86.0	6.5	3	7.5	4	10	10	12.5
470	86.0	6.8	1	2.5	6	15	10	12.5
471	86.4	6.5	4	10	5	12.5	14	17.5
472	87.0	6.3	4	10	6	15	10	12.5
473	87.0	6.6	3	7.5	5	12.5	10	12.5

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime	Post Lime		Alum
474	87.0	-		2.5	5	-	(ppm)	(I/min)
475	87.9		4		5	12.5	-	
476	88.0		4	10	7	17.5	11	13.75
477 478	88.0		2	5	5	12.5	10	12.5
478	88.0	_	0		5	12.5	10	12.5
480	89.0	6.6	4	101	6.0	15	13.0	12.5
481	89.0	6.5	3	7.5	5	12.5	10	16.25
482	89.0	6.8	1	2.5	5	12.5	10	12.5
483	89.0	5.8	7	17.5	5	12.5	10	12.5
484	90.0	6.5	5	12.5	6	15	15	12.5 18.75
485	90.0	6.6	3	7.5	6	15	10	12.5
486	90.0	6.9	1	2.5	5	12.5	10	12.5
487	91.0	5.9	6	15	5	12.5	10	12.5
488	91.0	6.7	2	5	7	17.5	10	12.5
489	91.0	6	0	0	5	12.5	10	12.5
490	91.3	6.5	6	15	5	12.5	10	12.5
491	92.0	6.8	5	12.5	6	15	10	12.5
492	92.0	5.8	1	2.5	5	12.5	11	13.75
493		6.1	7	17.5	5	12.5	11	13.75
494		6.9	5	12.5	6	15		13.75
495		5.9	1 Iniversit	2.5 V OF N45	5	anka 12.5		13.75
496		6.2	Electroni	15	5	12.5		13.75
497		6.6		12.0	DISSCI ₆	15		13.75
498	1000	6.5		mrt.aclot	6	15		16.25
499		6.4	5	10	5	12.5	14	17.5
500	94.0	7	0	12.5	5	12.5	14	17.5
501	94.0	6	- 6	0	6	15	11 -	13.75
502		3.3	4	15	5	12.5		3.75
503		5.5	4	10	6	15		3.75
504		5.2	7		5	12.5	13 1	6.25
505		.8	7	17.5 17.5	7.0		18.0	22.5
506		.1	5	12.5	6	15	11 1	3.75
507	95.0 6	.4	4	10	5	12.5	11 1	3.75
508	96.0 5	.9	6	15	7	17.5		3.75
509		.2	5	12.5	5	12.5	11 1	3.75
510		.5	3	7.5	0	0	11 1	3.75
511	97 6.		4	10	7	17.5		3.75
512		6	6	15	5	12.5	12	15
513	97.0 6.	3	4	10	6	15		3.75
514	97.0 6.	6	3	7.5	5	0		3.75
515	98.0 6.		5	12.5	5	12.5		.75
516	98.0 6.	1	5	12.5	7	12.5		7.5
					- 1	17.5	11 13	.75

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime (I/min)	Alum (ppm)	Alum (I/min)
517	98.0		4	10	0	0	11	-
518	98.0		2	5	5	12.5	11	
519	99.0		5	12.5	0	0	11	13.75
520	99.0	6.5	3	7.5	0	0	11	13.75
521	99.0	6.8	1	2.5	6	15	11	13.75
522	100.0	6.3	4	10	6	15	11	13.75
523	100.0	6.6	3	7.5	0	0	11	13.75
524	100.0	6.9	1	2.5	6	15	11	13.75
525	101.0	6.5	4	10	5	12.5	11	13.75
526	101.0	6.4	4	10	7	17.5	11	13.75
527	101.0	6.7	2	- 5	0	0	11	13.75
528	101.0	7	0	0	6	15	11	13.75
529	102	6.5	5	12.5	6	15	16	20
530	102.0	6.5	3	7.5	7	17.5	11	13.75
531	102.0	6.8	1	2.5	0	0	11	13.75
532	102.0	5.8	7	17.5	5	12.5	11	13.75
533	103.0	6.6	3	7.5	7	17.5	11	13.75
534	103.0	6.9	1	2.5	4	10	11	13.75
535	103.0	5.9	6	15	6	15	11	13.75
536	104	6.4	5	12.5	6	15	13	16.25
537	104.0	6.7	2	5	5	12.5	11	13.75
538	104.0	7	- Univeos	ity of Mo	ratuwa, 4	Lanka.10	11	13.75
539	104.0	6	Flect 6	ric The 15	& Disse	ations 15	11	13.75
540	105.0	6.5	4	10	5	12.5	11	13.75
541	105.0	6.8	WWW.	2.5	5	12.5	11	13.75
542	105.01	5.8	7	17.5	5	12.5	11	13.75
543	105.01	6.1	5	12.5	0	0	11	13.75
544	106.0	6.9	1	2.5	5	12.5	11	13.75
545	106.0	5.9	6	15	5	12.5	11	13.75
546	106.0	6.2	5	12.5	6	15	11	13.75
547	107.0	7	0	0	5	12.5	11	13.75
548	107.0	6	6	15	5	12.5	11	13.75
549	107.0	6.3	4	10	6	15	11	13.75
550	108.0	6.5	4	10	5	12.5	14	17.5
551	108.0	5.8	7	17.5	5	12.5	11	13.75
552	108.0	6.1	5	12.5	5	12.5	11	13.75
553	108.0	6.4	4	10	7	17.5	11	13.75
554		6.6	4	10	5	12.5	14	17.5
555	109.0	6.2	7	17.5	7.0	17.5	18.0	22.5
556	109.0	5.9	6	15	7	17.5	11	13.75
557	109.0	6.2	5	12.5	5	12.5	11	13.75
558	109.0	6.5	3	7.5	5	12.5	11	13.75
559	110	6.1	5	12.5	5	12.5	13	16.25



Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime (I/min)	Alum (ppm)	Alum (I/min)
560	110.0		6	15	7	17.5		13.75
561	110.0		4	10	5		11	13.75
562	110.0		3	7.5	6	15	11	13.75
563	111.0	_	5	12.5	7	17.5	11	13.75
564	111.0		4	10	5	12.5	11	13.75
565	111.0	6.7	2	5	6	15	11	13.75
566	112.0	6.5	4	10	5	12.5	11	13.75
567	112.0	6.2	5	12.5	6	15	11	13.75
568	112.0	6.5	3	7.5	5	12.5	11	13.75
569	112.0	6.8	1	2.5	5	12.5	11	13.75
570 571	113	6.5	4	10	5	12.5	13	16.25
572	113.0	6.3	4	10	5	12.5	11	13.75
573	113.0	6.6	3	7.5	5	12.5	11	13.75
574	113.0	6.9	1	2.5	7	17.5	11	13.75
575	114.0	6.5	4	10	5	12.5	14	17.5
576	114.0	6.4	4	10	6	15	12	15
577	114.0	6.7	2	5	5	12.5	12	15
578	115.0	6.5	0	0	5	12.5	12	15
579	115.0	6.5	4	10	5	12.5	11	13.75
580	115.0	6.8	3	7.5	6	15	12	15
581	115.0	7.1	-Univer	sity 0/2.5	ratuwa, 5	i Lan12.5	12	15
582	116.0	6.6	Elect ₃	nic 117.5	s & Discor	tations 15	12	15
583	116.0	6.9	WWW1	7.5	6	15	12	15
584	116.0	7.2	6	2.0	5	12.5	12	15
585	117	6.4	4	15	7	17.5	12	15
586	117.0	6.7	2	10	5	12.5	12	15
587	117.0	7	0	5	6	15	12	15
588	117.0	7.3	6	15	5	12.5	12	15
589	118	6.5	5	12.5	5	12.5	12	15
590	118.0	6.5	4	10	6	15	14.5	18.13
591	118.0	6.8	1	2.5	5	12.5	11	13.75
592	118.0	5.8	7	17.5	5	12.5	12	15
593	118.0	5.8	5	12.5	5	12.5	12	15
594	119.0	6.9	1	2.5	5	15	12	15
595	119.0	5.9	6	15	5	12.5	12	15
596		5.9	5	12.5	7	12.5	12	15
597		6.4	5	12.5	5	17.5	12	15
598	120.0	7	0	0	5	12.5	14	17.5
599	120.0	6	6	15	5	12.5 12.5	12	15
600		5.8	7	17.5	5	12.5	12	15
601	121.0	6.1	5	12.5	5	12.5	12	15
602	122.0	5.9	6	15	5	12.5	12	15 15

Sample No	Turbidity		Pre Lime (ppm)	Pre Lime (I/min)	Post Lime	Post Lime		Alum
603	122.0	6.2	5	12.5		12.5		-
604	123	6.5	5	12.5	6	12.5	12	
605	123.0	6.5	4	10	5	12.5	14	17.5
606	123.0	6	6	15	5	12.5	11	13.75
607	123.0	6.3	4	10	5	12.5	12	15
608	124	6.5	5	12.5	6	15.5	12	15
609	124	6.5	5	12.5	6	15	16	20
610	124	6.4	5	12.5	6	15	16	20
611	124.0	6.5	4	10	5	12.5	15	18.75
612	124.0	6.2	7	17.5	7.0	17.5	14	17.5
613	124.0	6.1	5	12.5	5	12.5	18.0	22.5
614	124.0	6.4	4	10	5	12.5	12	15
615	125	6	6	15	6	15	12	15
616	125	6.6	4	10	6	15	14	17.5
617	125.0	6.7	4	10	5	12.5	14	17.5
618	125.0	6.2	5	12.5	5	12.5	12	15
619	125.0	6.5	3	7.5	5	12.5	12	15
620	126.0	6.4	5	12.5	5	12.5	12	15
621	126.0	6.3	4	10	5		14	17.5
622	126.0	6.6	3	7.5	5	12.5	12	15
623	127.0	6.4	4	10	5	12.5 only 12.5	12	15
624	127.0	6.7	Univer2	y of Migla	tuwa, Sr	12.5	12	15
625	128.0	6.5	Electroni	c Thesto	The second second	12.5	12	15
626	128.0	6.5	www.13b.	mrt.a7.5	5	12.5	11	13.75
627	128.0	6.8	1	2.5	5	12.5	12	15
628	129.0	6.4	5	12.5	5	12.5	12	15
629	129.0	6.6	3	7.5	5	12.5	14	17.5
630		6.9	1	2.5	5	12.5	12	15
631	130.0	6.5	4	10	5		12	15
632	130.0	6.7	2	5	5	12.5	14	17.5
633	130.0	7	0	. 0	5	12.5	12	15
634	131.0	6.5	4	10	5	12.5	12	15
635	131.0	6.8	1	-	. 5		14	17.5
636	131.0	5.8	7	17.5	5	12.5	12	15
637	132	6.4	5	12.5	6	12.5	12	15
638	132.0	6.4	5	12.5	5	15		18.75
639	132.0	6.9	1	2.5	5	12.5	14	17.5
640	132.0	5.9	6	15	5	12.5	12	15
641	133.0	3.5	4	10	5	12.5	12	15
642	133.0	7	0	0	5	12.5	14	17.5
643	133.0	6	6	15	5	12.5	12	15
644		5.8	7	17.5	5	12.5	12	15
645		5.1	5	12.5	6	12.5	12	15

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime	Alum (ppm)	Alum (I/min)
646	135.0	5.9	6	15	6	15	12	. 15
647	135.0	6.2	5	12.5	5	12.5	12	15
648	136.0	6.5	4.	10	5	12.5	14	17.5
649	136.0	6	6	15	6	15	12	15
650	136.0	6.3	4	10	5	12.5	12	15
651	137.0	6.1	5	12.5	6	15	13	16.25
652	137.0	6.4	4	10	6	15	13	16.25
653	138.0	6.2	5	12.5	5	12.5	13	16.25
654	138.0	6.5	3	7.5	6	15	13	16.25
655	139	6.2	6	15	7	17.5	17	21.25
656	139	6.2	6	15	7	17.5	17	21.25
657	139.0	6.2	7	17.5	7.0	17.5	18.0	22.5
658	139.0	6.4	5	12.5	6	15	15	18.75
659	139.0	6.5	4	10	5	12.5	11	13.75
660	139.0	6.3	4	10	5	12.5	13	16.25
661 662	139.0	6.6	3	7.5	6	15	13	16.25
663	140.0	6.4	4	10	5	12.5	13	16.25
664	140.0	6.7	2	5	5	12.5	13	16.25
665	141.0 141.0	6.5	3	7.5	5	12.5	13	16.25
666	141.0	6.5	1	2.5	5	12.5	13	16.25
667	142.0	6.6	Unive ₃	sity of No	ratuwa, 5	Lank 12.5	11	13.75
668	142.0	6.9	Election	7.5	6	15	13	16.25
669	142.0	6.5	www6	2.5	5 00 101555	12.5	13	16.25
670	143	6.5	5	b.mrt.a ₁₅	5	12.5	14	17.5
671	143.0	6.7	2	12.5 5	5	12.5	14.5	18.13
672	143.0	7	0	0	6	15	13	16.25
673	144	6.4	6	15	5	12.5	13	16.25
674	144.0	6.8	1	2.5	5	12.5	14.5	18.13
675	144.0	5.8	7	17.5	5	15	13	16.25
676	145	6.3	5	12.5	5	12.5	13	16.25
677	145.0	6.9	1	2.5	6	12.5	16	20
678	145.0	5.9	6	15	5	15	13	16.25
679	146.0	7	0	0	6	12.5 15	13	16.25
680	146.0	6	6	. 15	5	12.5	13	16.25
681	147.0	5.8	7	17.5	6	15	13	16.25
682	147.0	6.1	5	12.5	5	12.5	13	16.25
683	148	6.6	5	12.5	6	15	13	16.25
684	148	6.3	6	15	5	12.5	16 16	20
685	148.0	5.9	6	15	6	12.5	13	20
686	148.0	6.2	5	12.5	5	12.5	13	16.25
687	149.0	6	6	15	6	15	13	16.25 16.25
688	149.0	6.3	4	10	5	12.5	13	16.25

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime (I/min)	Alum (ppm)	Alum (I/min)
689	150	5.8	7	17.5	6	15	14.5	18.13
690	150.0	6.1	5	12.5	6	15	13	16.25
691	150.0	6.4	4	10	5	12.5	13	16.25
692	151.0	6.2	5	12.5	6	15	13	16.25
693	151.0	6.5	3	7.5	5	12.5		16.25
694	152.0	6.3	4	10	6			16.25
695	152.0	6.6	3	7.5	5	12.5		16.25
696	153.0	6.4	4	10	6			16.25
697	153.0	6.7	2	5	5			16.25
698	154.0	6.5	3	7.5	6			16.25
699	154.0	6.8	1					16.25
700	155	6.4	4					
701	155.0	6.2	7					22.5
702	155.0	6.6						
703	155.0	6.9	1	2.5				
704	156.0	6.5	4	10				
705	156.0	6.7	2	5				
706	156.0	7						
707	157.0	6.8		2.5	6			
708		5.8	3	17.5				
709	158	6.6	Univer	ity of 12.		the last two districts	-	
710		6.9	Flectro	hic The	& Diese			
711	158.0	5.9) (15		7 17.5		
712	159	6.5	5 77 77 77 . 1	1. IIII t. a41		5 12.5		
713	159.0	6.5	5 4	1 10		5 12.		
714	159.0	6.6	6	4 1				
715	159.0) 7	7			5 12.		
716	159.0) (6	3 1		6 1		
717	7 160.0	5.8	3	7 17.		5 12.	_	
718				5 12.			5 14	
719	9 161.0	0 5.9	9	6 1	5	5 12.		_
720	0 161.	0 6.:	2	5 12.		7 17.		
72		0	6	6 1	5	5 12.		
72:	2 162.	0 6.	3	4 1		7 17.		
72	3 163.	C 6.	1	5 12.		5 12.		
72		C 6.	4	4 1	C		5 1	
72		4 6.	E		C	5] 12.		
72		0 6.	2.	5 12.		5] 12.		
72		0 6.	5	3 7		7] 17.		
72		_		4 1	0		15 1	
72			6	3 7	5			4 17.
73		_	4	4 1	0			4 17.
73		_	-7	2	5	3	15 1	4 17.

Sample No	Turbidity	рН	Pre Lime (ppm)	Pre Lime (I/min)	Post Lime (ppm)	Post Lime (I/min)	Alum (ppm)	Alum (l/min)
732	167.0	6.5	3	7.5	7	17.5	14	17.5
733	167.0	6.8	1	2.5	6	15	14	17.5
734	168	6.5	5	12.5	6	15	16	20
735	168.0	6.5	4	10	5	12.5	11	13.75
736		6.6	3	7.5	7	17.5	14	17.5
737	168.0	6.9	1	2.5	6	15	14	17.5
738		6.1	7	17.5	7.0	17.5	18.0	22.5
739		6.4	5	12.5	6	15	15	18.75
740	169.0	6.7	2	5	6	15	14	17.5
741	169.0	7	0	0	5	12.5	14	17.5
742	170.0		1	2.5	6	15	14	17.5
743		5.8	7	17.5	5	12.5	14	17.5
744	171	6.4	6	15	5	12.5	16	20
745		6.9	1	2.5	6	15	14	17.5
746		5.9	6	15	5	12.5	14	17.5
747	172.0	7	0	0	6	15	14	17.5
748			6	15	5	12.5	14	17.5
749		_	6	15	5	12.5	18	22.5
750	173.0	5.8	7	17.5			14	17.5
751	173.0		5	12.5		12.5	14	17.5
752		-	6	15	6	15	14	17.5
753		The same of the sa	Universi	12.5		12.5	14	17.5
754	The same of the sa		Electron6	c These ₁₅		1011S 17.5	14	17.5
755		_	www.lit4	mrt.ac.llo	5		14	17.5
756		-	7	17.5	6	15	14.5	18.13
757	176.0	-	5		7	17.5	14	17.5
758	176.0		4	10		12.5	14	17.5
759			5			17.5	14	17.5
760	177.0	6.5	3			12.5	14	17.5
761		_		10		12.5	14	17.5
762								17.5
763		-	4	-	5	12.5		15
764				10	5	12.5		
765			2					
766	-	-	+					
767		_				12.5		
768								
769								
770		_		17.5				
771		-						_
772								
773								+
774	183.0	5.8	7	17.5	5	12.5	15	18.75

				:				
Sample			Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(l/min)
775	184.0	6.9	1	2.5	6	15	15	18.75
776	184.0	5.9	6	15	5	12.5	15	18.75
777	185.0	7	0	0	6	15	15	18.75
778	185.0	6	6	15	5	12.5	15	18.75
779	186.0	5.8	7	17.5	6	15	15	18.75
780	186.0	6.1	5	12.5	5	12.5	15	18.75
781	187.0	5.9	6	15	6	15	15	18.75
782	187.0	6.2	5	12.5	5	12.5	15	18.75
783	188.0	6.4	5	12.5	6	15	15	18.75
784	188.0	6	6	15	6	15	15	18.75
785	188.0	6.3	4	10	5	12.5	15	18.75
786	189.0	6.1	5	12.5	6	15	15	18.75
787	189.0	6.4	4	10	5	12.5	15	18.75
788	190.0	6.2	5	12.5	6	15	15	18.75
789	190.0	6.5	3	7.5	5	12.5	15	18.75
790	191	6.2	7	17.5	7	17.5	18	22.5
791	191.0	6.2	7	17.5	7.0	17.5	18.0	22.5
792	191.0	6.3	4	10	6	15	15	18.75
793	191.0	6.6	3	7.5	6	15	15	18.75
794	192.0	6.4	4	10	6	15	15	18.75
795	192.0	6.7	2	sity of \5	6	15 1 ank 15	15	18.75
796	193.0	6.5	3	7.5	6	15	15	18.75
797	193.0	6.8	Election	2.5	S & DISS6	15	15	18.75
798	194.0	6.6	WWW3	1b.mrt.7.5	<u>K</u> 6	15	15	18.75
799	194.0	6.9	1	2.5	6	15	15	18.75
800	195.0	6.4	5	12.5	6	15	15	18.75
801	195.0	6.7	2	5	6	15	15	18.75
802	195.0	7	.0	0	5	12.5	15	18.75
803	196.0			2.5	6			
804			7	17.5	5	12.5		18.75
805	197	6.2	5	12.5	6	15		
806	197.0		1	2.5		15	1	18.75
807	197.0		6	15	5			
808	198.0		0	0	6	15		18.75
809			6	15	5	12.5		18.75
810	199.0		. 7	17.5		15		18.75
811	199.0		5	12.5	5	12.5	15	18.75
812	200		5					20
813	200.0	6.2	7	17.5				22.5
814	200.0	5.9	6	15	6	15	15	18.75
815	200.0	6.2	5				15	18.75
816	200.8		4		6		11	13.75
817	201.0	6	6	15	6	15	15	18.75

Sample			Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(l/min)
818	201.0	6.3	4	10	5	12.5	15	18.75
819	202.0	6.1	5	12.5	6	15	15	18.75
820	202.0	6.4	4	10	5	12.5	15	18.75
821	203	6.3	6	15	6	15	16	20
822	203.0	6.2	5	12.5	6	15	15	18.75
823	203.0	6.5	3	7.5	5	12.5	15	18.75
824	204.0	6.4	5	12.5	6.0	15	14.5	18.13
825	204.0	6.3	4	10	5	12.5	16	20
826	204.0	6.6	3	7.5	5	12.5	16	20
827	205.0	6.4	4	10	5	12.5	16	20
828	205.0	6.7	2	5	5	12.5	16	20
829	206.0	6.5	3	7.5	5	12.5	16	20
830	206.0	6.8	1	2.5	5	12.5	16	20
831	207.0	6.6	3	7.5	5	12.5	16	20
832	207.0	6.9	1	2.5	5	12.5	16	20
833	208.0	6.7	2	5	7	17.5	16	20
834	208.0	7	0	0	5	12.5	16	20
835	209	6.4	5	12.5	6	15	16	20
836	209.0	6.8	1	2.5	7	17.5	16	20
837	209.0	5.8	7	17.5	5	12.5	16	20
838	210.0	6.9	LInive1	ity of 2.5	ratuwa 4	i Lank 17.5	16	20
839	210.0	5.9	6	15	5	12.5	16	20
840	211.0	7	Electro	ine Theso	s & Disse	17.5	16	20
841	211.0	6	WWW.6	0.HIII.a45	5	12.5	16	20
842	212.0	5.8	7	17.5	6	15	16	20
843	212.0	6.1	5	12.5	5	12.5	16	20
844	213.0	5.9	6	15	5	12.5	16	20
845	213.0	6.2	5	12.5	5	12.5	16	20
846	214.0	6.5	4	10	5	12.5	12	15
847	214.0	6	6	15		17.5	16	20
848	214.0	6.3		. 10		12.5	16	20
849	215.0	6.1	5	12.5	6	15	16	20
850	215.0	6.4	4	10	5	12.5	16	20
851	216.0	6.4	5	12.5	6.0	15	14.5	18.13
852	216.0			12.5		15	16	20
853	216.0	6.5	3	7.5		12.5	16	20
854	217.0			10	6		16	20
855	217.0	6.6		7.5			16	20
856	218.0	6.4		10		15	16	20
857	218.0	6.7	2	. 5			16	20
858	219.0		3			15	16	20
859	219.0	-		2.5			16	20
860	220.0	6.6	3	7.5	6	15	16	

			con l					
Sample	birlity	oH		Pre Lime	Post Lime		Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(l/min)
861	220.0	6.9	1	2.5	6.0	15	16	20
862	221.0	6.7	2	- 5	6	15	16	20
863	221.0	7	0	0	6.0	15	16	20
864	222.0	6.4	5	12.5	6.0	15	14.5	18.13
865	222.0	6.8	1	2.5	6	15	16	20
866	222.0	5.8	7	17.5		15	16	20
867	223.0	6.9	·1	2.5	6	15	16	20
868	223.0	5.9	6	15		15	16	20
869	224.0	6.4	5	12.5	6.0	15	14.5	18.13
870	224.0	7	0	0	6	15	16	20
871	224.0	6	6	15	6.0	15	16	20
872	225	6.3	6	15	5	12.5	17	21.25
873	225.0	5.8	7	17.5	6	15	16	20
874	225.0	6.1	5	12.5	6.0	15	16	20
875	226.0	5.9	6	15	6	15	17	21.25
876	226.0	6.2	5	12.5	7.0	17.5	17	21.25
877	227.0	6	6	15	6	15	17	21.25
878	227.0	6.3	4	10	7.0	17.5	17	21.25
879	228.0	6.1	5	12.5	6	15	17	21.25
880	228.0	6.4	4	10	7.0	17.5	17	21.25
881	229.0	6.2	5	12.5	6	15	17	21.25
882	229.0	6.5	Univeg	ity of 7.5	ratuwa,7.0	Lanka7.5	17	21.25
883	230	6.2	Electr4	nic The 10	s & Disses	ations 12.5	14	17.5
884	230.0	6.3	www.4	b.mrt.at0	6	15	17	21.25
885	230.0	6.6	3	7.5	7.0	17.5	17	21.25
886	231.0	6.4	4	10	6	15	17	21.25
887	231.0	6.7	2	5	7.0	17.5	17	21.25
888	232.0	6.5	3	7.5	6	15	17	21.25
889	232.0	6.8	1	2.5	7.0	17.5	17	
890			3	7.5				21.25
891	233.0	6.9	1	· 2.5	7.0			
892	234.0	6.3	5	12.5	5	12.5	15	
893	234.0	6.7	2	5				21.25
894	234.0	7	0	0	7.0			21.25
895	235.0	6.8	1	2.5	5			21.25
896	235.0	5.8	7	17.5			17	21.25
897	236.0		. 1	2.5			17	21.25
898	236.0			15			17	21.25
899	237.0	_	0				17	21.25
900	237.0						17	21.25
901	238.0	-	7				17	21.25
902		_	5				17	21.25
903		_					17	21.25

Sample			Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(I/min)	(ppm)	(I/min)
904	239.0	6.2	5	12.5	7.0	17.5	17	
905	240.0	6	6	15	6	15	17	21.25
906	240.0	6.3	4	10	7.0	17.5	17	21.25
907	241.0	6.1	5	12.5	6	15	17	21.25
908	241.0	6.4	4	10	7.0	17.5	17	21.25
909	242.0	6.2	5	12.5	6	15	17	21.25
910	242.0	6.5	3	7.5	7.0	17.5	17	21.25
911	243.0	6.3	4	10	6	15	17	21.25
912	243.0	6.6	3	7.5	5	12.5	17	21.25
913	244.0	6.4	4	10	6	15	17	21.25
914	244.0	6.7	2	5	5	12.5	17	21.25
915	245.0	6.5	3	7.5	6	15	17	21.25
916	245.0	6.8	1	2.5	5	12.5	17	21.25
917	246.0	6.6	3	7.5	6	15	17	21.25
918	246.0	6.9	1	2.5	5	12.5	17	21.25
919	247.0	6.7	2	5	6	15	17	21.25
920	247.0	7	0	0	5	12.5	17	21.25
921	248.0	6.8	1	2.5	6	15	18	22.5
922	248.0	5.8	7	17.5	5	12.5	18	22.5
923	249.0	6.9	1	2.5	6	15	18	22.5
924	249.0	5.9	6	15	5	12.5	18	22.5
925	250.0	7	Univer9	y of Moo	ituwa, Sr6	Lanka. 15	18	22.5
926	250.0	6	Electro6	c Thesd5	& Disser5	ions 12.5	18	22.5
927	251.0	6.2	5	12.5	5	12.5	15	18.75
928	251.0	5.8	7	17.5	6	15	18	22.5
929	251.0	6.1	5	12.5	5	12.5	18	22.5
930	252.0	5.9	6	15	6	15	18	22.5
931	252.0	6.2	5	12.5	5	12.5	18	22.5
932	253.0	6	6	15	6	15	18	22.5
933	253.0	6.3	4	10	5	12.5	18	22.5
934	254.0	6.1	5	12.5	6	15	18	22.5
935	254.0	6.4	4	10	5	12.5	18	22.5
936	255.0	6.4	5	12.5	5	12.5	15	18.75
937	255.0	6.2	5	12.5	6	15	18	22.5
939	255.0	6.5	3	7.5	5	12.5	18	22.5
	256.0	6.3	4	10	6	15	18	22.5
940	256.0 257.0	6.6	3	7.5	5	12.5	18	22.5
941	257.0	6.4	4	10	6	15	18	22.5
942	258.0	6.7	2	5	5	12.5	18	22.5
943	258.0	6.4	5	12.5	5	18	15	18.75
944	258.0	6.5	3	7.5	6	15	18	22.5
946	259.0	6.8	1	2.5	5	12.5	18	22.5
340	238.0	0.0	3	7.5	6	15	18	22.5

Sample			Pre Lime	Pre Lime	Post Lime	Post Lime	Alum	Alum
No	Turbidity	рН	(ppm)	(l/min)	(ppm)	(l/min)	(ppm)	(l/min)
947	259.0	6.9	1	2.5	5	12.5	18	22.5
948	260.0	6.7	2	5	5	12.5	18	22.5
949	260.0	7	0	0	5	12.5	18	22.5
950	261.0	6.8	1	2.5	5	12.5	18	22.5
951	261.0	5.8	7	17.5	5	12.5	18	22.5
952	262.0	6.9	1	2.5	5	12.5	18	22.5
953	262.0	5.9	6	15	5	12.5	18	22.5
954	263.0	7	0	0	0	0	18	22.5
955	263.0	6	6	15	5	12.5	18	22.5
956	264.0	5.8	7	17.5	7	17.5	18	22.5
957	264.0	6.1	5	12.5	5	12.5	18	22.5
958	265.0	5.9	6	15	7	17.5	18	22.5
959	265.0	6.2	5	12.5	5	12.5	18	22.5
960	266.0	6	6	15	7	17.5	18	22.5
961	266.0	6.3	4	10	5	12.5	18	22.5
962	267.0	6.1	5	12.5	6	15	18	22.5
963	267.0	6.4	4	10	5	12.5	18	22.5
964	268.0	6.2	. 5	12.5	7	17.5	18	22.5
965	268.0	6.5	3	7.5	5	12.5	18	22.5
966	269.0	6.3	4	. 10	6	15	18	22.5
967	269.0	6.6	Univers 3	y of M7.5	tuwa, Sr5	Lanka12.5	18	22.5
968	270.0	6.4	Electron4	c These 10	& Disser5	tions 12.5	18	22.5
969	270.0	6.7	1112	mrt ac 115	5	12.5	18	22.5
970	271.0	6.5	3	7.5	5	12.5	19	23.75
971	271.0	6.8	1	2.5	5	12.5	19	23.75
972	272.0	6.6	3	7.5	5	12.5	19	23.75
973	272.0	6.9	1	2.5	5	12.5	19	23.75
974	273.0	6.7	2	5	5	12.5	19	23.75
975	273.0	7	0	0	5	12.5	19	23.75
976	274.0	6.8	1	. 2.5	5	12.5	-	
977	274.0	5.8	7	17.5	6	15	19	23.75
978	275.0	6.9	1	2.5	5	12.5	19	23.75
979	275.0	5.9	6	15	6	15	19	23.75
980	276.0	7	0	0	5	12.5	19	
981	276.0	6	6	15				
982	277.0	5.8	7	17.5				
983		-	-	-				
984								
985		-					-	
986								
987		_						
988		-					-	
989		_	-					

Sample No	Turbidity	рН	Pre Lime (ppm)		Post Lime (ppm)	Post Lime (I/min)	Alum (ppm)	Alum (I/min)
990	282.0	6.3	4	10	5	12.5	19	
991	283.0	6.4	4	10	5	12.5	19	
992	284.0	6.5	3	7.5	5	12.5	19	23.75
993	285.0	6.6	3	7.5	5	12.5	19	23.75
994	286.0	6.7	2	5	5	12.5	19	23.75
995	287.0	6.8	1	2.5	5	12.5	19	23.75
996	288.0	6.9	1	2.5	5	12.5	19	23.75
997	289.0	7	0	0	5	12.5	19	23.75
998	290.0	5.8	7	17.5	5	12.5	19	23.75
999	291.0	5.9	6	15	5	12.5	19	23.75
1000	292.0	6	6	15	5	12.5	19	23.75

Note: All Turbidity values are in NTU.



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Appendix-B

Filtered SPH Final Water Vater SPH Rel Tdty pH Rel Tdty													P	uality	Quality of Water	ater								
Minimal Mini									S	ettled	Wate	_					Filte	pa			Final	Water		
Main			Lime	Alum	Puls	ator	Pul.t	aqn	Cfloc	k-1	Cfloc	k-2	PT		PT	7	Wat	- La		SPH			Kubot	
66 7.5 11.34 1.1 6.2 2.6 2.6 1.5 1.6 2.2 6.6 1.5 1.1 0.5 7.2 8.6 7.5 11.34 1.1 6.4 1.2 6.2 2.6 2.6 2.6 2.1 6.0 6.4 0.6 7.7 1.1 0.5 7.2 8.66 7.5 11.36 1.3 6.4 1.8 </th <th>Tdty</th> <th>- 1</th> <th>(F)</th> <th>5</th> <th>Tdty</th> <th>Hd</th> <th>Tdty</th> <th>Hd</th> <th>Tdty</th> <th>Hd</th> <th>Tdty</th> <th>-</th> <th>\perp</th> <th></th> <th></th> <th>-</th> <th>Tdty</th> <th></th> <th></th> <th>E</th> <th>Rel</th> <th>Tdty</th> <th>Hd</th> <th>Rel</th>	Tdty	- 1	(F)	5	Tdty	Hd	Tdty	Hd	Tdty	Hd	Tdty	-	\perp			-	Tdty			E	Rel	Tdty	Hd	Rel
66 7.5 11.31 1.6 2.0 64 1.8 6.4 1.8 <td>24.2</td> <td>6.6</td> <td></td> <td></td> <td>-</td> <td>6.9</td> <td></td> <td>109</td> <td>1,0</td> <td>63</td> <td>1.6</td> <td>- 0</td> <td>,</td> <td>1</td> <td>1.</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>	24.2	6.6			-	6.9		109	1,0	63	1.6	- 0	,	1	1.									
66 7.5 11.34 1.1 64 2.0 64 1.8 62 1.8 64 1.8 64 1.8 64 1.8 64 1.1 64 7.5 11.36 11.36 1.3 1.4 1.3 1.3 1.4 1.3 1.4	23.4	9.9			?	7.0		7.0	7.7	7.0	-	7.0	7:7	7.0	7.1	7.0			0.5		=	0.5		=
66 75 1136 1 64 12 64 18 64 19 64 18 64 18 64 18 64 18 64 18 64 18 64 18 64 18 64 18 64 18 64 18 64 18 64 19 64 18	24.2	9.9			1.1	6.4	2.0	6.4	5.1	62	22	6.2	~	6.2	1-	6.7	0	7,7	-		1	0	t	1
6 6 7.5 11.38 1.3 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.8 6.4 1.1 0.0 7.1 1.1 0.0 7.2 1.1 0.0 7.2 1.1 0.0 7.2 1.1 0.0 7.2 1.1 0.0 7.2 1.1 0.0 </td <td>24.8</td> <td>9.9</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>7:</td> <td>1</td> <td>4.0</td> <td>2</td> <td>4.0</td> <td>1.7</td> <td>7.0</td> <td>0.0</td> <td>4.0</td> <td>D.4</td> <td></td> <td>2:1</td> <td>0.8</td> <td>7.7</td> <td>1.0</td>	24.8	9.9								7:	1	4.0	2	4.0	1.7	7.0	0.0	4.0	D.4		2:1	0.8	7.7	1.0
666 7.5 11.39 64 1.3 62 2.6 1.8 64 1.7 64 0.7 6.4 0.7 0.4 0.7 1.1 0.9 0.7 0.7 0.7 0.7 0.7 0.7 0.7 0.1 1.1 0.9 0.7 0.7 0.1 0.1 0.7 0.7 0.1 0.1 0.7 0.7 0.1 0.1 0.7 0.7 0.1 0.1 0.7 0.7 0.1 0.1 0.7 0.7 0.1 0.1 0.7 0.1 0.2 0.2 0.2 1.2 0.2 1.2 0.2 1.2 0.2	25.4	9.9		11.38	1.3	6.4	1.8	6.4	2.2	6.4		6.4	~	44	×	7,4	10	+	-	-	1	0	t	
6.65 7.5 11.31 1.3 6.4 1.3 6.4 2.3 6.2 1.6 1.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.4 7.0 1.1 1.0 7.5 6.65 7.5 11.32 1.05 6.4 1.1 6.4 1.7 6.4 1.7 6.4 0.4 7.4 0.8 0.9 7.3 6.6 7.5 11.32 1.0 6.4 1.2 6.4 1.4 6.4 0.7 6.4 0.4 7.1 1.0 1.1 7.2 6.7 5 11.32 1.0 6.2 2.2 6.2 1.8 6.2 1.2 0.2 1.2<	25.7	9.9		11.39					EI	Uı			1:0	5	0.1	÷	5	4,0	4.0	=	1	0.9	7.7	0.8
6.65 7.5 11.32 1.05 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.1 6.4 1.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4 6.4 0.4	23.5	6.65		11.31	1.3	6.4	1.9	6.4	23	6.2	2.6	62		6.4	17	19	10	7	0 0	10	-	-	1	1
6.65 7.5 11.32 1.05 6.4 1.1 6.4 2.0 6.2 1.7 6.2 1.6 1.7 6.1 6.4 0.4 7.1 1.0 0.4 7.3 1.1 7.2 6.6 7.5 11.32 1.4 6.4 1.2 6.2 2.2 6.2 1.8 6.4 1.4 6.4 0.7 6.4 0.7 1.1 1.1 7.2 6.7 5 11.32 1.0 6.2 3.2 </td <td>23.6</td> <td>6.65</td> <td>7.5</td> <td>11.32</td> <td></td> <td></td> <td></td> <td>-</td> <td>tro</td> <td>er</td> <td></td> <td>+</td> <td></td> <td>+</td> <td>+</td> <td></td> <td>3</td> <td>,</td> <td>2</td> <td>,</td> <td>1</td> <td>2.1</td> <td>C.</td> <td>1.0</td>	23.6	6.65	7.5	11.32				-	tro	er		+		+	+		3	,	2	,	1	2.1	C.	1.0
66 7.5 11.32 14 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 64 12 65 12 65 13 65 13 62 <th< td=""><td>23.7</td><td>6.65</td><td></td><td>11.32</td><td>1.05</td><td>6.4</td><td>Ξ</td><td>6.4</td><td>2.0</td><td></td><td>2.4</td><td>6.2</td><td>17</td><td>6.2</td><td>19</td><td>62</td><td>10</td><td>79</td><td>7</td><td>1</td><td>0</td><td>0</td><td>1,</td><td> -</td></th<>	23.7	6.65		11.32	1.05	6.4	Ξ	6.4	2.0		2.4	6.2	17	6.2	19	62	10	79	7	1	0	0	1,	-
66 7.5 11.32 1.4 6.4 1.2 6.4 1.5 6.2 1.8 6.4 1.4 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.4 0.7 6.7 0.7 <td>23.7</td> <td>9.9</td> <td></td> <td>11.32</td> <td></td> <td></td> <td></td> <td>m</td> <td>0</td> <td></td> <td></td> <td></td> <td>+</td> <td>+</td> <td></td> <td></td> <td></td> <td>5</td> <td>-</td> <td>-</td> <td>0.5</td> <td>0.7</td> <td>?</td> <td></td>	23.7	9.9		11.32				m	0				+	+				5	-	-	0.5	0.7	?	
67 5 1132 1 62 3.2 62 3.2 6.2	23.6	9.9	7.5	11.32	1.4	6.4	-	6.4	1.9	6.2	2.2	6.2	~	6.4	1	19	0.7	14	5	-	-	1	1	1
6.7 5 11.32 1.09 6.2 3.7 6.2 3.2 6.2 <td>23.6</td> <td>6.7</td> <td>5</td> <td>11.32</td> <td></td> <td></td> <td>_</td> <td>1C</td> <td>es</td> <td>М</td> <td></td> <td>+</td> <td>+</td> <td>+</td> <td>+</td> <td>5</td> <td>3</td> <td>+</td> <td>;</td> <td>+</td> <td>1</td> <td></td> <td>7:7</td> <td>0.9</td>	23.6	6.7	5	11.32			_	1C	es	М		+	+	+	+	5	3	+	;	+	1		7:7	0.9
6.7 5 11.33 1 6.2 3.9 6.2 1.8 6.2 2.9 6.2 0.4 0.4 0.4 0.4	23.7	6.7	5	11.32	1.09	6.2	~	6.2	1.	6.2	1.9	6.2		6.2	3.2	62	T	+	T	\dagger	T		T	
6.7 5 11.34 1 6.2 3.9 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.4 6.2 3.5 6.2 3.4 6.2 3.5 6.2 1.7 6.2 1.7 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.3 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2 3.5 6.2	23.9	6.7	5	11.33					&	atı				+	+	+	40	109	40	1-	-	100	0 4	-
6.7 5 11.35 6 2.9 6.2 3.6 6.2 2.5 6.2 0.4 0.4	24.2	6.7	5	11.34	-	6.2	6	6.2	1.7	6.2	8.1	6.2	3.4	6.2	2.9	6.5		-		+	2	3		
6.7 5 11.47 0.98 6.2 2.9 6.2 1.7 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 3.6 6.2 1.7 6.2 3.7 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.3 6.4 6.3 6.4 6.3 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 <td>24.6</td> <td>6.7</td> <td>5</td> <td>11.35</td> <td></td> <td></td> <td></td> <td></td> <td>IS</td> <td>a,</td> <td></td> <td></td> <td></td> <td>-</td> <td></td> <td>\dagger</td> <td></td> <td>+</td> <td>T</td> <td>+</td> <td>\dagger</td> <td>T</td> <td>T</td> <td></td>	24.6	6.7	5	11.35					IS	a,				-		\dagger		+	T	+	\dagger	T	T	
6.7 5 11.48 6.7 <td>28.1</td> <td>6.7</td> <td>5</td> <td>11.47</td> <td>0.98</td> <td>6.2</td> <td>6</td> <td>6.2</td> <td>1.7</td> <td>6.2</td> <td></td> <td>6.2</td> <td></td> <td>6.2</td> <td>25</td> <td>6.2</td> <td></td> <td>62</td> <td>\v</td> <td></td> <td></td> <td>10</td> <td>1</td> <td>-</td>	28.1	6.7	5	11.47	0.98	6.2	6	6.2	1.7	6.2		6.2		6.2	25	6.2		62	\v			10	1	-
6.7 5 11.52 11.12 11.12 11.12 11.12 11.12 11.12 11.12 11.12 11.12 11.13 11.14	28.3	6.7	5	11.48				-	ta	i		-		+		+		1	3			5	1	-
6.7 5 11.43 6.8 3.1 6.3 1.5 6.3 2.8 6.3 0.4 6.2 0.5 7.3 4.0 0.7 6.9 6.7 5.1 11.39 1.47 6.8 3.1 6.8 1.5 6.3 1.5 6.3 2.8 6.3 6.4 6.3 6.3 6.4 6.3 6.4 6.4 6.4 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 <td>29.6</td> <td>6.7</td> <td>5</td> <td>11.52</td> <td>1.12</td> <td>6.2</td> <td></td> <td>6.2</td> <td>1.8</td> <td>6.2</td> <td></td> <td>6.2</td> <td></td> <td>6.2</td> <td>2.7</td> <td>6.2</td> <td>T</td> <td>+</td> <td>\dagger</td> <td>+</td> <td>\dagger</td> <td>T</td> <td>T</td> <td></td>	29.6	6.7	5	11.52	1.12	6.2		6.2	1.8	6.2		6.2		6.2	2.7	6.2	T	+	\dagger	+	\dagger	T	T	
6.7 5 11.39 1.47 6.8 3.1 6.3 1.5 6.3 2.8 6.4 3.0 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.4 6.5 7.2 <td>27.1</td> <td>6.7</td> <td>5</td> <td>11.43</td> <td></td> <td></td> <td></td> <td>-</td> <td>ns</td> <td>nk</td> <td></td> <td>-</td> <td></td> <td>-</td> <td>+</td> <td>+</td> <td>┪</td> <td>5</td> <td>20</td> <td>1 2</td> <td>-</td> <td>0</td> <td>10,9</td> <td> -</td>	27.1	6.7	5	11.43				-	ns	nk		-		-	+	+	┪	5	20	1 2	-	0	10,9	-
6.7 5 11.34 1 6.4 3.4 6.4 3.0 6.4 0.4 6.4 3.0 6.4 0.4 6.4 3.0 6.4 0.4 6.4 3.0 6.4 0.4 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.9 6.5 4.0 6.5 4.2 6.4 4.5 6.5 4.6 6.5 4.9 6.5 4.0 6.5 4.0 6.5 4.0 6.5 4.0 6.5	25.9	6.7	5	11.39	1.47	8.9	—	5.8	1.9	6.3	_	6.3				6.3	+	7.		+	2	<u> </u>	6.0	2
6.7 5 11.33 1.56 6.4 3.2 6.4 2.1 6.4 1.4 6.4 3.4 6.4 3.0 6.4 6.4 6.4 6.4 74 1.1 0.8 7.0 7.0 7.0 7.0 7.0 7.0 7.0 7.0 7.0 7.0	24.2	6.7	5	11.34	-			-	-			-		L			T	+	\dagger	+	\dagger		+	
6.6 7.5 12.61	23.9	6.7	5	11.33	1.56	6.4	7	5.4	2.1	6.4		6.4				44		+	-	7	+	0	10	-
6.5 7.5 12.45 2.3 6.6 3.8 6.4 4.7 6.6 4.8 6.6 4.9 6.5 4.9 6.5 7.8 1.1 6.6 1.0 7.6 1.0 0.9 7.3 1.4 6.6 7.5 12.41 1.78 6.6 4.0 6.5 5.1 6.6 4.3 6.6 3.7 6.5 4.6 6.5 1.1 6.6 1.0 7.6 1.0 0.9 7.3 1.4 6.6 7.5 12.34 1.4 6.6 4.3 6.4 5.7 6.6 4.3 6.6 3.7 6.5 6.5 1.1 6.6 1.0 7.6 1.0 7.6 1.0 7.8 1.3 1.4 6.6 4.3 6.4 5.1 6.5 2.1 6.5	59.6	9.9	7.5	12.61				-	-			-				+		+	-	+	+	0	;	-
6.6 7.5 12.44 6.6 5.1 6.6 4.0 6.5 5.1 6.6 4.2 6.5 6.4 6.5 7.5 12.41 1.78 6.6 4.0 6.5 5.1 6.6 4.2 6.5 4.6 6.5 7.5 12.34 1.49 6.6 4.2 6.4 5.7 6.6 4.3 6.6 3.7 6.5 4.6 6.5 1.1 6.6 1.0 7.6 1.0 0.9 7.3 1.40 6.6 4.2 6.4 5.7 6.6 4.3 6.6 3.7 6.5 2.8 6.5 1.2 6.5 1.1 6.6 1.0 7.6 1.0 7.6 1.0 7.7 1.2 7.3 1.40 6.6 4.3 6.4 5.1 6.5 2.2 6.5 2.1 6.5 2.8 6.5 1.2 6.6 1.0 7.6 1.0 7.6 1.0 7.7 1.2 7.3 1.40 6.5 1.3 6.5	55.4	6.5	7.5	12.45	2.3	9.9		5.4	4.7	9.9	~	9.9				15.9	\dagger	+	\dagger	+	\dagger	1	+	
6.6 7.5 12.41 1.78 6.6 4.0 6.5 5.1 6.6 4.5 6.6 4.2 6.5 4.6 6.5 1.1 6.6 1.0 7.6 1.0 7.7 1.2 1.2 1.2 1.2 1.2 1.2 1.2 1.2 1.2 1.2	55.0	9.9	7.5	12.44		-		-	-	-	_	-		\perp			+-	9		14	-	0	1,2	-
6.6 7.5 12.34 6.6 4.2 6.4 5.7 6.6 4.3 6.6 2.1 6.5 2.1 6.5 2.8 6.5 1.2 6.6 1.0 7.6 1.0 7.8 1.0	54.2	9.9	7.5	-		9.9				9.9	_		\perp		\perp	14	+	2			7:1	7.7	7	2.1
6.6 7.5 12.33 1.49 6.6 4.2 6.4 5.7 6.6 4.3 6.6 3.7 6.5 4.6 6.5 1.1 6.6 1.0 7.6 1.0 0.9 7.3 6.6 6.6 7.5 12.41 6.6 4.3 6.4 2.1 6.5 2.2 6.5 2.1 6.5 2.8 6.5 1.2 6.6 1.0 7.6 1.0 7.6 1.0 7.8 7.3	52.4	9.9	7.5	12.34		-	-		_	-	_		L	上		3	\dagger	+	\dagger	+	+	\dagger	\dagger	
6.6 7.5 12.41 6.6 7.3 13.27 1.73 6.6 4.3 6.4 2.1 6.5 2.2 6.5 2.1 6.5 2.8 6.5 1.2 6.6 1.0 7.6 1.0 1.0 7.3	52.1	9.9	7.5			9.9	_	4	-	9.9	_					4	+	1		191	-	0	1,	-
6.6 7.5 13.27 1.73 6.6 4.3 6.4 2.1 6.5 2.2 6.5 2.1 6.5 2.8 6.5 1.2 6.6 1.0 76 1.0 7 1.0 73	54.3	9.9	7.5	12.41		-	-		\vdash				L		\perp	+	-	2		2	-	6:5	7	2.1
	76.4	9.9	7.5						L	6.5					_	5.5	_	9			0	-	7 3	0

_				_					Sottle	Sottled Wet			Cuainy of Water	y or v	ater								
		Lime	Alum	Pu	Pulsator	-	Pul.tube	Cffe	Cflock-1	U water	er ck2	Da		1		Filte	Filtered			Final	Final Water		
Ldty	Hd	(I/min)	(I/min)	Tdt	lty pH		Ha	Tdf	E	12		Tar		4		Water	ter		SPH			Kubota	"
156.0	6.5	7.5	16.85	2.	_	-		,	1	- 4-	-	rary		Idty	Hd	Tdty	pH	Tdty	Hd	Rel	Tdtv	Hu	Pel
133.0	6.5	7.5	15.73						Co	7 7	0.0	2.9	6.5	3.6	6.5	1.4	9.9	1.2	8.0	1.0	-	7.2	1
124.0	6.5	7.5		2	8 64	4	4.4	2.7	1	ľ	-											1	
131.0	6.5	7.5					-	i	0.0	7.4	6.5	4.1	9.9	4.6	9.9	1.3	9.9	0.4	7.1	10	1.4	7.0	10
130.0	6.5	7.5		1.84	4 64	40	7		1		_								1			2.	
114.0	6.5	7.5		_			_	3.1	0.7	3.2	9.9	4.3	9.9	4.6	9.9	1.3	9.9	0.5	7.3	0	1 2	10	
0.801	6.5	7.5		161	14	10	0 /	3													C.1	0.7	1.0
93.4	6.5	7.5	13.97			5.0	C:O	3.9	6.5	3.8	9.9	4.6	9.9	4.9	9.9	1.4	9.9	0.7	74	0	13	1	
86.4	6.5	7.5	13.68	157	6.0		N	eĠ	ni	1							1		-	2	CT	0./	1.0
79.2	6.5	7.5	13.38		1	0	0.4	1	6.5	3.4	9.9	4.6	9.9	4.8	9.9	1.2	9.9	0.7	7.4	10	1=	10	-
76.1	6.5	7.5	13.26	1 52	4.4	10	100	o d	rs		1						-		1	+		?	
66.4	6.5	7.5	12.87			3.7	4.	4	6.5	3.2	9.9	4.7	9.9	5.1	9.9	1.3	9.9	0.7	7.4	0	1.2	7.0	10
65.1	9.9	7.5	12.82	174	6.0	20			6	1	+	1							+	-	1	?!	
1.99	9.9	7.5	12.86	1.1		7.0	0.0	7	0.9	3.8	0.9	5.9	0.9	4.9	0.9	1.3	0.9	1.0	7.4	6.0	10	7.2	-
0.68	9.9	7.5	13.78			1	14.	esi	M	1	+	1					-		-		111	4:	1.1
159.0	9.9	7.5	17.00	1.4	4.4	1	1		or	-	+					0.8	6.5	1.0	7.5	0	90	13	10
204.0	6.4	10	19.37				6.0	N	6.4	5.3	6.4	3.8	6.4	3.9	6.5		-		-		2	5.	
222.0	6.4	10	20.39			1	+	1	ulv	+	+	+	1			0.8	6.4	8.0	7.4	1.0	90	73	10
224.0	6.4	10	20.50	1.7	64	=	6.1) [5	va		1	1	+						-	-	-	+	1
216.0	6.4	10	20.05			-	-	36	4.0.4	7.8	6.4	3.6	6.5	3.9	6.5	6.4 0	0.1	1.0	7.4	1.0	9.0	74	10
200.0	6.2	12.5	19.15	4.3	5.9	3.4	0.9	0.9	0	_					-				-	-	-	+	-
191.0	6.2	12.5	18.66			_		200		10.3	5.9	0.1	0.9	7.2	0.9					-	+	+	
182.0	6.2	12.5	18.18	4.0	6.2	3.1	63	0	25	0 1				_	+	1		4.6 7	7.4 0	6.0	2.6	7.4	-
0.691	6.1	12.5	17.50			_		SIS	7:00	-	7.0	0.8	2.9	6.3	6.2	+	+	+				-	
155.0	6.2	12.5	16.80	3.1	6.2	3.6	63	5.0	6.3	00						+	4			_		-	
139.0	6.2	12.5	16.02	-	-				7.0	_	7.0	5.3	6.2	5.9	6.2	1.1 6.	6.2	1.8 7.	7.8 0	6.0	1.3	7.2	10
124.0	6.2	12.5	15.32	3.1	6.2	3.8	63	40	63	63					+	1				-		-	
109.0	6.2	12.5	14.64	-						_	0.7	4.9	6.2	5.5 6	6.2	-					-	+	
Y	6.2	12.5	14.04	2.9	6.2	3.4 62		3.1	6.3	1-		\perp	_	1		1.2 6.2		1.4 8.	2 0.9		1.8	7.8	=
	FE 6.3	10	13.66	-		_				2.4 0.7		4.2	6.2 4	4.4	6.2	-						-	
	55 6.3	10	13.13	3.2	6.2	3.7 6.2		29	62	6.1 6		\perp			1	\rightarrow					-	-	
67.0	6.3	10	12.90			_				0.4 0.7		4.8	6.2	4.8 6.2	2 1	.2 6.2		1.4 8.1	6.9	9	.4	-	1.0
64.0	6.3	10	12 78	20	63	25 60	\perp	0	1	1		4		_	_	_		_	L		-	+	

																-							
									Settle	Settled Water	1.					Filtered	red			Final	Final Water		
		Lime	Alum	Pulsa	sator	Pul	Pul.tube	U U	Cflock-1	Cflock-2	ck-2	PTI	1	P	PT2	Water	er		SPH			Kubota	
Tdty	Hd	(I/min)	(I/min)	1 -	pH	Tdty	y pH	Tdty	Hd	Tdty	Hd	Tdty	Ηd	Tdty	Hd	Tdty	Ηd	Tdty	Hd	Rel	Tdty	Hd	Rel
0.09	6.4	10	12.63	2.8	6.4	3.	4 6.4	3.8	6.4	4.4	6.4	4.4	6.4	4.6	6.4	1.1	6.4	1.2	7.4	0.9	0.7	7.2	=
9.7	8.9		10.79	1.0	6.5	0.6	5 6.5	3.7	9.9	1.5	9.9	1.7	9.9	1.9	9.9	1.2	6.7	2.1	6.9	0.8	0.8	7.1	0.8
7.6	8.9		10.79								- 11												
7.7	8.9	5	10.79	0.7	6.5	0	9 6.5	1.2	6.5	0.0	9.9	1.0	6.5	1.4	6.5	1.1	6.7	1.4	7.3	0.9	0.8	7.5	0.9
7.7	8.9		10.79					The same	-														
7.7	8.9		10.79	0.7	6.5	0	9 6.5	1.6	6.5	0.0	9.9	1.6	6.5	1.4	6.5	1.0	6.7	0.8	7.9	0.9	0.8	8.0	0.9
9.7	6.9	2.5	10.79																				
7.5	6.9		10.79	8.0	6.5	1.08	8 6.5	1.8	6.5	1.2	9.9	1.8	6.5	2.2	6.5	1.0	6.7	0.9	7.9	6.0	0.8	8.0	0.9
7.3	6.9	2.5	10.78				, v	lle	Jn			-											
7.3	6.9	2.5	10.78	8.0	6.5		5 6.5	1.8	6.3	1.2	9.9	2.4	6.5	2.7	6.5	0.9	0.7	0.7	9.7	0.9	0.8	7.8	0.9
7.3	6.9	2.5	10.78	*			. 4.4	ro 13	er														
7.4	6.9	2.5	10.78				٥.	ni L	sit														
7.5	6.9	2.5	10.79	0.8	6.5		5 6.5	G n	6.5		9.9	2.2	6.5	2.5	6.5								
7.5	6.9	2.5	10.79					Ch	of							0.9	6.7	0.7	7.8	0.9	0.7	7.4	0.9
7.5	6.9	2.5	10.79					es	M														
7.4	6.9	2.5	10.78	0.8	6.5	1.6	5 6.5	= 130	6.5	1.0	9.9	2.1	6.5	2.3	6.5	8.0	6.7	0.7	7.8	6.0	0.7	7.4	0.9
7.3	6.9	2.5	10.78					8	at														
7.2	6.9	2.5	10.78	0.8	6.5	1.4	4 6.5	0.9	6.5	1.0	9.9	1.9	6.5	2.1	8.9	8.0	6.7	0.7	7.8	0.9	0.6	7.3	0.9
13.2	6.5	7.5	10.97					Dis	va														
13.9	9.9	7.5	10.99	1.6	6.4	1.9	9 6.4	1.6	6.4	1.6	6.4	1.5	6.4	2.4	6.4								
15.1	6.6	7.5	11.03					rt	ri									9.0	7.8	0.9	0.4	7.7	=
24.3	6.7	5	11.34					ati	L														
41.9	6.7		11.95					01	ar														
57.3	6.8	5	12.52					1S	ıkı									0.5	8.0	8.0	0.5	7.7	1.2
87.9	6.8	5	13.74						1.														
125.0	6.7		15.36																				
179.0	9.9	7.5	18.02															0.7	8.1	8.0	0.5	7.7	1.0
214.0	6.5	7.5	19.93																				
255.0	6.4	10	22.36																				
258.0	6.4	10	22.54															0.5	8.0	0.80.89	_	7.6	0.8
251.0	6.2	12.5	22.11																				
234.0	6.3	10	21.09																				
												Ì								ł			

												ý	Hanny	Quality of water	er							
								Š	Settled Water	Water					F	Filtered	_		F	Final Water	er	
		Lime	Alum	Pulsator	ator	Pul.tube	npe	Cflock-1		Cflock-2	c-2	PT1		PT2		Water		SPH	=		Kubota	Ē
Tdty	Hd	(I/min)	(I/min)	Tdty	Hd	Tdty	Hd	Tdty	Hd	Tdty pH		Tdty	pH 1	Tdty p	pH T	Tdty pH	H Tdty	ty pH	H Rel	Tdty	v pH	Rel
132.0	6.4	10	15.69														_					
129.0	6.4	10	15.55								-			-	-	-	-	\vdash	-	L	L	L
126.0	6.4	10	15.41											-	-	-	-	\vdash	-		-	
120.0	6.4	10	15.13								-				-	-	-	\vdash	L			
0.86	6.4	10	14.16				Total Control		40					-		-	-	+	-		-	L
94.0	6.4	10	13.99)	37					+	-		-	\vdash			L	
43.0	6.5	7.5	11.99)		-	-	\vdash		-	-	-	-	\vdash			_	
40.1	6.5	7.5	11.89	1.3	6.2	2.2	6.2	2.0	6.2	1.6	6.2	2.0	6.2	1.9	6.2	0.8	6.4	0.8 7.3	3 1.1	L	0.9 7.2	
38.5	6.5	7.5	11.83				W	16	In						-	-				L		
37.4	6.5	7.5	11.79	1.1	6.4	2.0	6.4	1.9	6.2	2.2	6.2	1.8	6.2	2.1	6.2	0.8	6.4 0.	7.1	1.0	0.8	8 7.2	1.0
35.5	6.5	7.5	11.73				.1	ro	er						-	-		\vdash				
41.2	6.5	7.5	11.93	1.3	6.4	1.8	6.4	2.2	6.4	2.4	6.4	1.8	6.4	1.8	6.4	0.7 6.4	0	2.7		0.0	9 7.7	0 8
41.4	6.5	7.5	11.94				m	C'	V		-				+	+		\vdash		L		
49.3	6.5	7.5	12.22	1.3	6.4	1.9	6.4	2.3	6.2	2.6	6.2	1.8	6.4	1.7	6.4	0.7 6.4	4	\vdash			_	L
57.0	6.5	7.5	12.51				ac	les	N					-	-	-		6.0			L	
123.0	6.5	7.5	15.27	1.05	6.4	1.1	6.4	2.0	6.2	2.4	6.2	1.7	6.2	1.6	6.2	0.7 6.4	4	-	-	L	L	L
139.0	6.5	7.5	16.02				Z	8	ra				-			-		-		L	L	
168.0	6.5	7.5	17.45	1.4	6.4	1.2	6.4	1.9	6.2	2.2	6.2	8.1	6.4	1.4	6.4	0.7 6.4		0.9 7.1	1.0		1 7.2	0.9
142.0	6.5	7.5	16.16					Di	W		-			-	-	-					\perp	
128.0	6.5	7.5	15.50	1.09	6.2	3.7	6.2	123	6.2	1.9	6.2	3.2	6.2	3.2 6	6.2	-		-			L	
118.0	6.5	7.5	15.04				-	er	Sr			-				0.4 6.2		0.9 7.1	1.0	0	7 6.9	1.0
115.0	6.5	7.5	14.91	1	6.2	3.9	6.2	1.7	6.2	1.8	6.2	3.4	6.2	2.9 6	6.2			-			L	
112.0	6.5	7.5	14.77					io	a		_					-		-				
105.0	6.5	7.5	14.47	86.0	6.2	2.9	6.2	1.7	6.2	1.7	6.2	3.6	6.2	2.5 6	6.2	0.4 6.2		0.9 7.2	0.0	0	7 7.0	=
101.0	6.5	7.5	14.29					L.	a			-		-								
45.8	6.5	7.5	12.10	1.12	6.2	3.3	6.2	1.8	6.2	1.8	6.2	3.3	6.2	2.7 6	6.2	-		-		L		
91.3	6.5	7.5	13.88												F	0.4 6.2	2	0.9 7.3	4.0	0	7 6.9	10
85.7	6.5	7.5	13.65	1.47	8.9	3.1	8.9	1.9	6.3	1.5	6.3	3.4	6.3	2.8 6.	6.3	-		\vdash				
80.2	6.5	7.5	13.42									-	-	-	-	-		-	L			
77.0	6.5	7.5	13.29	1.56	6.4	3.2	6.4	2.1	6.4	1.4	6.4	3.4	6.4	3.0	6.4	0.4 6.4		10 74	E	8	7.0	-

Appendix-C

Setting up Peripherals

Before writing the setting up code for the devices, all the constants that have to be used in the source code have been defined. Apart from that a set of variables are defined to make it easier to access memory locations.

#define	up		2
#define	down		1
count	0×21		
packet	0×22		
temp	0×23		
digit1	0×24		
digit2	0×25		
digit3	0×26		
digit4	0×27		
digit5	0×28		
digit6	0×29		
digit7	$0 \times 2A$		
digit8	0×2B	T	University of Moratuwa, Sri L
	1300		Electronic Theses & Dissertat
Status_ter	np 🧺	equ	0×2C
t1		equ	0×2D mrt.ac.lk
t2		equ	0×2E
+2			

t3 equ $0 \times 2F$ L_byte equ 0×30 H_byte equ 0×31 R0equ 0×32 R1 equ 0×33 R2 equ 0×34 t4 equ 0×35 t5 equ 0×36 t6 equ 0×37 minimum equ 0×38 maximum equ 0×39 counter equ $0 \times 3A$ cur_turbidity equ $0 \times 3B$ set_turbidity equ $0 \times 3C$ w_turbidity equ $0 \times 3D$

time equ $0\times3E$ pclath_turbidity equ $0\times3F$ flag equ 0×40

send_spi

macroaddress, no

;macro for SPIsending

movlw

address

call

data_send

movlw

no

call

data send

endm

The include file PIC16F876.inc is included to let the MPLAB compiler to understand which device of the family is being used.

include "PIC16F876.inc"

_config _cp_off&_WDT_OFF&_BODEN_off&_PWRTE_off&_XT_osc

list

At the beginning of the device the port and variable initialization step starts. The following code fragment depicts what are the registers that have to be initialized in this manner. Reset vector and Interrupt vector originating locations are mentioned with two 'goto' lables.

org 0×000

goto start

org 0×004

start

;timer1 interrupts used with internal oscillator, MAX7219 display

banksel TRISC

movlw b'00000011'

movwf TRISC

movlw 0×FF

movwf TRISB

clrf TRISA

bsf

TRISA,1

banksel

OPTION_REG

clrf OPTION REG bsf OPTION REG,7 bsf PIE1,0 banksel **PORTC** clrf **PORTC** clrf **PORTA** clrf **PORTB** clrf ADCON0 movlw 0×0 D movlw T1CON clrf flag clrf TMR1H clrf TMR1H clrf TMR1L movlw 0×02 movwf time movlw $0 \times C0$ movwf **INTCON** clrf PIR1 movlw 0×0 F movwf digit1 movwf digit2 digit3 movwf movwf digit4 digit5 movwf movwf digit6 movwf digit7 movwf digit8 Initialize banksel ADCON0 ;RA1 input is the Analog input proportional to turbidity movlw 0×49 movwf ADCON0 clrf PIR1 banksel ADCON1

movlw

movwf

 0×84

ADCON1

clrf	ADRESL
banksel	ADRESH
clrf	ADRESH
clrf	H_byte
clrf	L_byte

SPI

banksel **SSPSTAT** clrf **SSPSTAT** banksel **SSPCON** movlw 0×30 movwf **SSPCON** movlw 0×02 movwf packet

Start

banksel **PORTB**

clrf **PORTB** ; clear PORTB

movlw B'01000001' ; Fosc/8, A/D enabled

banksel OPTION REG movlw B'10000111'

; TMR0 prescaler, 1:256 (20µs) lıb.mrt.ac.lk

movwf OPTION REG

movwf ADCON0

clrf TRISB ; PORTB all outputs

movlw B'00001110' ; Left justify, 1 analog channel movwf ADCON1 ; VDD and VSS references

banksel **PORTB**

Main

btfss INTCON, TOIF ; Wait for Timer0 to timeout

goto Main

bcf INTCON, TOIF

bsf ADCON0,GO ; Start A/D conversion

Wait

btfss PIR1,ADIF ; Wait for conversion to complete

goto Wait

movf ADRESH,W ; Write A/D result to PORTB movwf **PORTB**

	clrf	PORTB	
send_tur			; sends current turbidity to the display
	movelw	$0 \times 0F$	
	andwf	R2,w	
	movwf	digit1	
	swapf	R2,f	
	movlw	$0\times0F$	
	andwf	R2,w	
	movwf	digit2	
	movlw	0×0 F	
	andwf	R1,w	
	movwf	digit3	
	movlw	0×FF	
	andwf	digit3,1	
	btfss	STATUS,2	
	goto	test_tur1	
	movlw	0×0F	
1	movwf	digit3	f Moratuwa, Sri Lanka.
test_tur1			heses & Dissertations
	movlw	U^IT	
	andwf btfss	digit2,1	
		STATUS,2	
test tur2	goto	send_tur1	
test_turz	movelw	OVOE	
	xorwf	0×0F	
	btfss	digit3,0	
	goto	STATUS,2	
	movlw	send_tur1 0×0F	
	movwf		
send tur1	1110 A AA1	digit2	
	movlw	0×04	
	call	data_send	
	movf	digit4,0	
	call	data_send	; dig1 data
	movly	0×02	

0×03

data_send

call movlw

call

```
movf
                            digit3,0
                                                                 ; dig2 data
             call
                            data_send
             movlw
                            0\times02
             call
                            data_send
             movf
                            digit2,0
                                                                 ; dig3 data
             call
                            data_send
             movlw
                            0 \times 01
             call
                            data_send
            movf
                            digit1,0
                                                                 ; digl data
            call
                            data send
            return
 send initial
                                          ; sends initial turbidity to the display
            movelw
                           0 \times 0F
            andwf
                           R2,w
            movwf
                           digit5
            swapf
                           R2,f
            movlw
                           0 \times 0F
            andwf
                           R2,w
            movwf
                           digit6
            movlw
                           0 \times 0F
                           Riversity of Moratuwa, Sri Lanka.
            andwf
                           digit7 Theses & Dissertations
            movwf
                          www.lib.mrt.ac.lk
            movlw
                           0 \times FF
            andwf
                           digit7,1
           btfss
                           STATUS,2
           goto
                          test_initial1
           movlw
                          0 \times 0F
           movwf
                          digit7
test_initial1
           movlw
                          0 \times FF
andwf
                          digit6,1
           btfss
                          STATUS,2
           goto
                          send_initial1
test initial2
           movelw
                          0 \times 0F
           xorwf
                          digit7,0
           btfss
                          STATUS,2
           goto
                          send_initial1
```

	movlw	0×0F	
	movwf	digit6	
seno	d_initial1	8	
	movlw	0×08	
	call	data send	•
	movf	digit8,0	1.1.1.1
	call	data_send	; digl data
	movlw	0×07	
	call	data send	
	movf	digit7,0	11.0.1
	call	data_send	; dig2 data
	movlw	0×06	
	call	data_send	
	movf	digit5,0	
	call	data_send	; dig3 data
	movlw	0×05	
	call	data send	
	movf	digit1,0	
call	data_send	argiti,0	; digl data
	return		
	ADC	University of Electronic Twww.lib.mr	and assessed to 1 '1'
	banksel	ADCON0	
	bsf	ADCON0,2	
	goto loop	11200110,2	
	C		
loop			
•	btfss	PIR1,6	
	goto	loop	
	bcf	PIR1,6	
	banksel	ADRESH	
	movf	ADRESH,w	
	movwf	H_byte	
	rrf	H_byte, I	
	banksel	ADRESL	
	movf	ADRESL,w	
	banksel	L_byte	
	movwf	L_byte	

L_byte

movwf

rrf	H_byte,1
movlw	0×01
andwf	H_byte,1
movf	L_byte,0
movwf	cur_tur

return

compare

;routine used to compare current turbidity with initial turbidity

movf	cur_tur,0
subwf	ini-tur,0
btfss	STATUS,1
goto	ON
goto	compare

end





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Appendix-D					
Turbidity (NTU)	Dossage (I/min)	Movement (°)	Turbidity (NTU)	Dossage (I/min)	Movement (°)
4	10.20	91.8	54	12.87	115.9
5	10.25	92.3	55	12.93	116.4
6	10.30	92.7	56	12.99	116.9
7	10.35	93.2	57	13.04	117.4
8	10.40	93.6	58	13.10	117.9
9	10.45	94.1	59	13.16	118.4
10	10.51	94.6	60	13.22	118.9
11	10.56	95.0	61	13.27	119.5
12	10.61	95.5	62	13.33	120.0
13	10.66	95.9	63	13.39	120.5
14	10.71	96.4	64	13.45	121.0
15	10.76	96.9	65	13.50	121.5
16	10.82	97.3	66	13.56	122.1
17	10.87	97.8	67	13.62	122.6
18	10.92	98.3	68	13.68	123.1
19	10.97	98.7	69	13.74	123.6
20	11.02	99.2	70	13.79	124.1
21	11.08	99.7	71	13.85	124.7
22	11.13	100.2	72	13.91	125.2
23	11.18	100.6	73	13.97	125.7
24	11.23	101.1	74	14.03	126.3
25	11.29	101.6	75	14.09	126.8
26	11.34	102.1	76	14.15	127.3
27	11.39	102.5	77	14.21	127.9
28	11.45 nive	rsity 103.0/ora	hiwa 78ri Lar	14.27	128.4
29	11.50	103.5	79	14.32	128.9
30	11.55	104.0	Dissipliation	14.38	129.5
31	11.61WW	104.5 lk	81	14.44	130.0
32	11.66	104.5	82	14.50	130.5
	11.72	105.4	83	14.56	131.1
33		105.4	84	14.62	131.6
34	11.77	106.4	85	14.68	132.2
35	11.82				
36	11.88	106.9	86	14.74	132.7
37	11.93	107.4	87	14.80	133.2
38	11.99	107.9	88	14.86	133.8
39	12.04	108.4	89	14.93	134.3
40	12.10	108.9	90	14.99	134.9
41	12.15	109.4	91	15.05	135.4
42	12.21	109.9	92	15.11	136.0
43	12.26	110.3	93	15.17	136.5
44	12.32	110.8	94	15.23	137.1
45	12.37	111.3	95	15.29	137.6
46	12.43	111.8	96	15.35	138.2
47	12.48	112.3	97	15.41	138.7
48	12.54	112.8	98	15.48	139.3
49	12.59	113.3	99	15.54	139.8
50	12.65	113.9	100	15.60	140.4
51	12.71	114.4	101	15.66	141.0
52	12.76	114.9	102	15.72	141.5
53	12.82	115.4	103	15.79	142.1

Turbidity (NTU)	Dossage (I/min)	Movement (°)	Turbidity (NTU)	Dossage (I/min)	Movement (°)
104	15.85	142.6	155	19.19	172.7
105	15.91	143.2	156	19.26	173.3
106	15.97	143.8	157	19.33	174.0
107	16.04	144.3	158	19.40	174.6
108	16.10	144.9	159	19.47	175.2
109	16.16	145.5	160	19.54	175.8
110	16.23	146.0	161	19.61	176.4
111	16.29	146.6	162	19.67	177.1
112	16.35	147.2	163	19.74	177.7
113	16.42	147.7	164	19.81	178.3
114	16.48	148.3	165	19.88	179.0
115	16.54	148.9	166	19.95	179.6
116	16.61	149.5	167	20.02	180.2
117	16.67	150.0	168	20.02	180.8
118	16.74	150.6	169	20.09	181.5
119	16.80	151.2	170		
				20.23	182.1
120	16.86	151.8	171	20.30	182.7
121	16.93	152.4	172	20.38	183.4
122	16.99	152.9	173	20.45	184.0
123	17.06	153.5	174	20.52	184.6
124	17.12	154.1	175	20.59	185.3
125	17.19	154.7	176	20.66	185.9
126	17.25	155.3	177	20.73	186.6
127	17.32	155.9	178	20.80	187.2
128	17.38	156.4	179	20.87	187.9
129	17.45	157.0	180	20.94	188.5
130	17.51 Uni	vers1157.6 Mo	ratuw1815r1 La	nka.21.02	189.1
131	17.58 Fled	from 158.2 leses	& D182-rtatio	ons 21.09	189.8
132	17.65	158.8	183	21.16	190.4
133	17.71	159.4	184	21.23	191.1
134	17.78	160.0	185	21.30	191.7
135	17.84	160.6	186	21.38	192.4
136	17.91	161.2	187	21.45	193.0
137	17.98	161.8	188	21.52	193.7
138	18.04	162.4	189	21.59	194.3
139	18.11	163.0	190	21.67	195.0
140	18.18	163,6	191	21.74	195.6
141	18.24	164.2	192	21.81	196.3
142	18.31	164.8	193	21.88	197.0
143	18.38	165.4	194	21.96	197.6
144	18.44	166.0	195	22.03	198.3
145	18.51	166.6	196	22.10	198.9
146	18.58	167.2	197	22.10	
					199.6
147	18.65	167.8	198	22.25	200.3
148	18.71	168.4	199	22.33	200.9
149	18.78	169.0	200	22.40	201.6
150	18.85	169.7	201	22.47	202.3
151	18.92	170.3	202	22.55	202.9
152	18.99	170.9	203	22.62	203.6
153	19.05	171.5	204	22.70	204.3
154	19.12	172.1	205	22.77	204.9

Turbidity (NTU)	Dossage (I/min)	Movement (°)	Turbidity (NTU)	Dossage (I/min)	Movement (°)
206	22.85	205.6	253	26.49	238.4
207	22.92	206.3	254	26.57	239.1
208	23.00	207.0	255	26.65	239.9
209	23.07	207.6	256	26.73	240.6
210	23.15	208.3	257	26.81	241.3
211	23.22	209.0	258	26.89	242.0
212	23.30	209.7	259	26.97	242.8
213	23.37	210.3	260	27.06	243.5
214	23.45	211.0	261	27.14	244.2
215	23.52	211.7	262	27.22	245.0
216	23.60	212.4	263	27.30	245.7
217	23.68	213.1	264	27.38	246.4
218	23.75	213.8	265	27.46	247.2
219	23.83	214.4	266	27.55	247.9
220	23.90	215.1	267	27.63	248.6
221	23.98	215.8	268	27.71	249.4
222	24.06	216.5	269	27.79	250.1
223	24.13	217.2	270	27.87	250.9
224	24.21	217.9	271	27.96	251.6
225	24.29	218.6	272	28.04	252.4
226	24.36	219.3	273	28.12	253.1
227	24.44	220.0	274	28.20	253.8
228	24.52	220.7	275	28.29	254.6
229	24.60	221.4	276	28.37	255.3
230	24.67	222.1	277	28.45	256.1
231	24.75	222.8	278	28.54	256.8
232	24.83	223.5	279	28.62	257.6
233	24.91 Llec	TOT 224.2 leses	& D280 rtati	DIS 28.70	258.3
234	24.99	116 224.9 ac 1	281	28.79	259.1
235	25.06	225.6	282	28.87	259.8
236	25.14	226.3	283	28.96	260.6
237	25.22	227.0	284	29.04	261.4
238	25.30	227.7	285	29.12	262.1
239	25.38	228.4	286	29.21	262.9
240	25.46	229.1	287	29.29	263.6
241	25.53	229.8	288	29.38	264.4
242	25.61	230.5	289	29.46	265.2
243	25.69	231.2	290	29.55	265.9
244	25.77	231.9	291	29.63	266.7
245	25.85	232.7	292	29.72	267.4
246	25.93	233.4	293	29.80	268.2
247	26.01	234.1	294	29.89	269.0
248	26.09	234.8	295	29.97	269.7
249	26.17	235.5	296	30.06	270.5
250	26.25	236.3	297	30.14	271.3
251	26.33	237.0	298	30.23	272.1
252	26.41	237.7	299	30.31	272.8

